

NOTATION:

Th:

Ē.G.,

 $T_c$ :

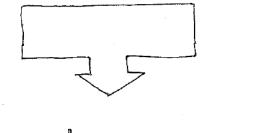
BULLDOG PIPE

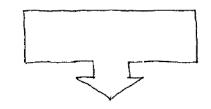
(IN):

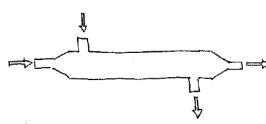
(OUT);

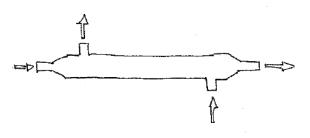
Thin =

# TWO ARRANGEMENTS









# ASSUMPTIONS FOR ANALYSIS:

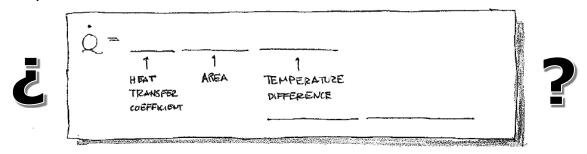
1)

3)

2)

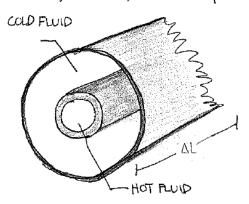
4)

WE WOULD LIKE A HEAT TRANSFER COEFFICIENT THAT, CIVES & BETWEEN THE TWO FLUIDS FOR THE WHOLE HXR\*



HOW DO WE FIND U?

FOR A SMALL SECTION of HXR:



SIDE VIEW DF INNER TUBE

Th

TUSE TE

δġ = \_\_\_\_\_

WHERE

R<sub>TOTAL</sub> =

50:

UA =

MUST CHOOSE AN AREA ON WHICH TO BASE U:

UA=

\_\_ USUALLY BASED ON AREA

MNYWAY...

STILL NEED

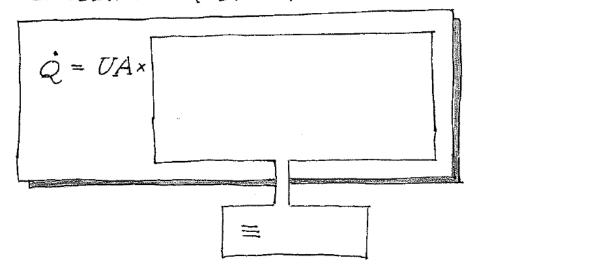
 $\dot{Q} = UA \Delta T_{AVL} = UA (T_n - T_c)_{AVL}$  = ?

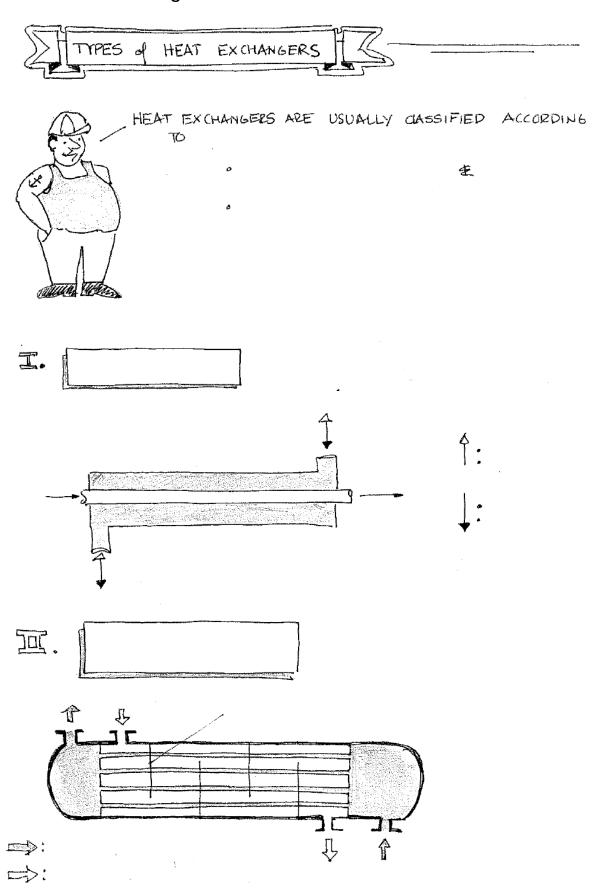
PROBLEM:

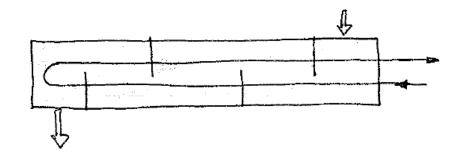
SOLUTION:

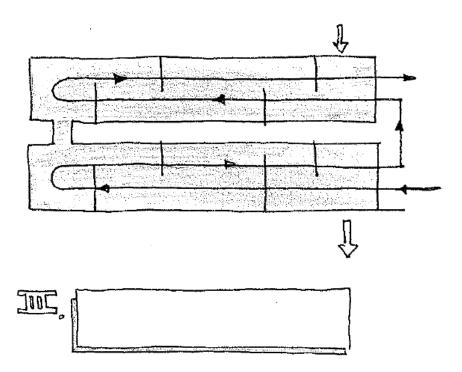
ASSUMPTION # 5:

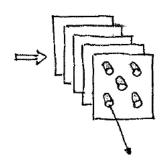
CONSERVATION of ENERGY + ASSUMPTION # 5 YIELDS

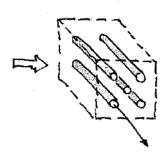






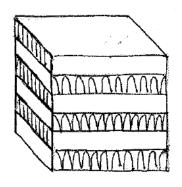


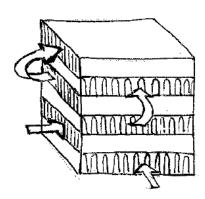














Q= UA\*AT, WAS DERIVED FOR A DOUBLE-PIPE HXR.

Answer: YES, IF....



WHERE

F= f(

R = \_\_\_\_\_

P = \_\_\_\_\_