

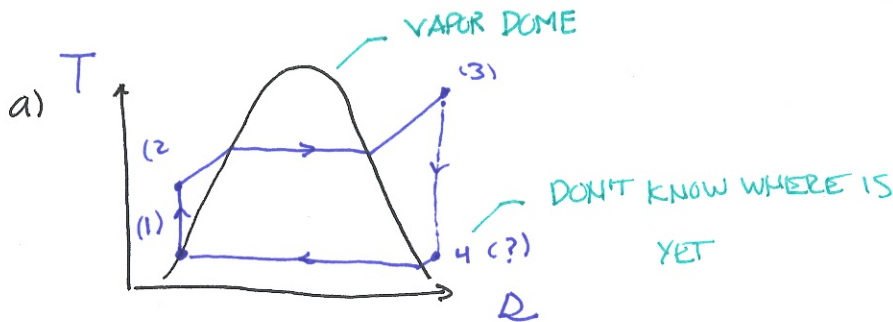
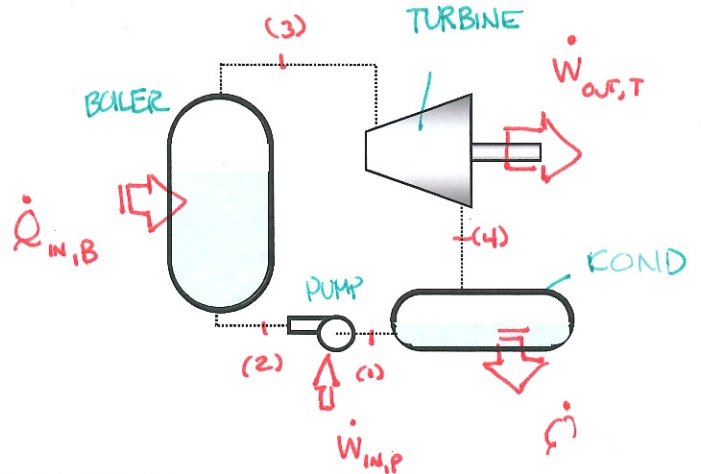
NOT (IDEAL IMPLIES $x_3 = 1$ too!)

Example

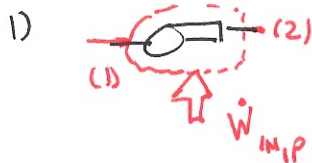
SO IT'S ALMOST IDEAL!

An ideal Rankine cycle operates with a boiler pressure of 8 MPa and a condenser pressure of 10 kPa. The liquid entering the pump is saturated, and the vapor entering the turbine has a temperature of 700°C. The mass flow rate of steam through the cycle is 1 kg/s.

- Sketch the cycle on a $T-s$ diagram.
- Calculate:
 - the power into the pump,
 - the heat transfer into the boiler,
 - the power out of the turbine, and
 - the heat transfer rejected by the condenser.
- Find the efficiency of the cycle.



b) PUMP:



$$\frac{dE}{dt} = \dot{Q}_{in} + \dot{W}_{in,P} + \dot{m}(h_1 + \dots) - \dot{m}(h_2 + \dots)$$

$$\dot{W}_{in,P} = \dot{m}(h_2 - h_1)$$

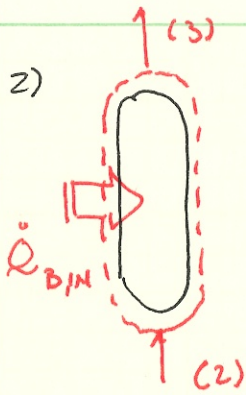
$$h_1 = h(10 \text{ kPa}, x=0) = \underline{191.7 \text{ kJ/kg}}$$

$$s_1 = s(10 \text{ kPa}, x=0) = \underline{0.6489 \text{ kJ/kg}}$$

$$h_2 = h(8 \text{ MPa}, s_2 = s_1) = \underline{199.8 \text{ kJ/kg}}$$

$$\begin{aligned} \dot{W}_{in,P} &= (1 \text{ kg/s}) \left(199.8 \frac{\text{kJ}}{\text{kg}} - 191.7 \frac{\text{kJ}}{\text{kg}} \right) \\ &= 8.058 \text{ kW} \end{aligned}$$

$$w_{in,P} = \frac{\dot{W}_P}{\dot{m}} = 8.058 \text{ kJ/kg}$$



$$\frac{dE_{sys}}{dt} = \dot{Q}_{IN} + \dot{L}_0 + \dot{m}(h_2 + \dots) - \dot{m}(h_3 + \dots)$$

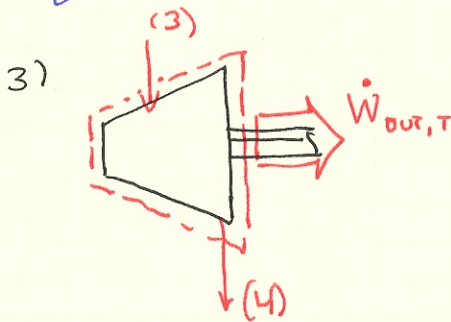
$$\dot{Q}_{IN,B} = \dot{m}(h_3 - h_2)$$

$$q_{IN,B} = \frac{\dot{Q}_{IN,B}}{\dot{m}} (h_3 - h_2)$$

$$h_3 = h(700^\circ\text{C}, 8 \text{ MPa})$$

$$= \underline{3881 \text{ kJ/kg}}$$

$$q_B = \dots = 3682 \text{ kJ/kg}$$



$$\dot{L}_0 = \dot{L}_0 - \dot{W}_{OUT,T} + \dot{m}(h_3 + \dots) - \dot{m}(h_4 + \dots)$$

$$\dot{W}_{OUT,T} = \dot{m}(h_3 - h_4)$$

$$W_{OUT,T} = (h_3 - h_4)$$

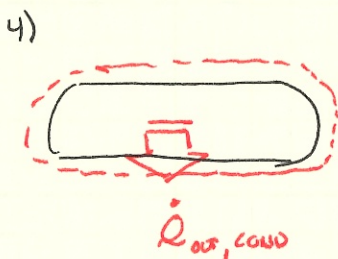
$$P_3 = P(700^\circ\text{C}, 8 \text{ MPa}) = \underline{7.28 \text{ kJ/kg}\cdot\text{K}}$$

$$h_4 = h(10 \text{ kPa}, P_4 = P_3)$$

$$= \underline{2307. \text{ kJ/kg}}$$

< $h_g(10 \text{ kPa})$ IT IS A MIXTURE!!

$$W_{OUT,T} = 1575 \text{ kJ/kg}$$



$$\dot{L}_0 = -\dot{Q}_{OUT,C} + \dot{L}_0 + \dot{m}(h_4 + \dots) - \dot{m}(h_1 + \dots)$$

$$q_{OUT,COND} = \frac{\dot{Q}_{OUT,C}}{\dot{m}} = (h_4 - h_1)$$

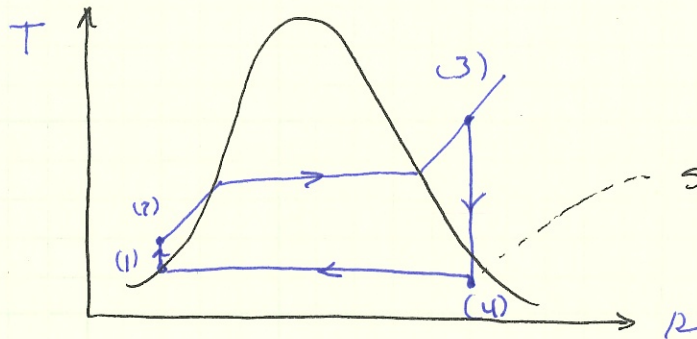
$$= \dots = 2115 \text{ kJ/kg}$$

$q_{OUT,COND}$ SHOULD ALSO BE $q_{IN,B} - (W_{OUT,T} - W_{IN,P})$. WHY?

$$c) \quad \eta_{TH} \equiv \frac{\dot{W}_{NET,OUT}}{\dot{Q}_H} = \frac{W_{NET,OUT}}{q_{IN}} = \frac{W_{T,OUT} - W_{P,IN}}{q_{IN,B}} = \dots$$

$$= 0.426 = 42.6\%$$

CORRECTED T-s DIAGRAM



STATE (4) IS A MIXTURE

SINCE $h_4 < h_g (10 \text{ RPa})$

Example

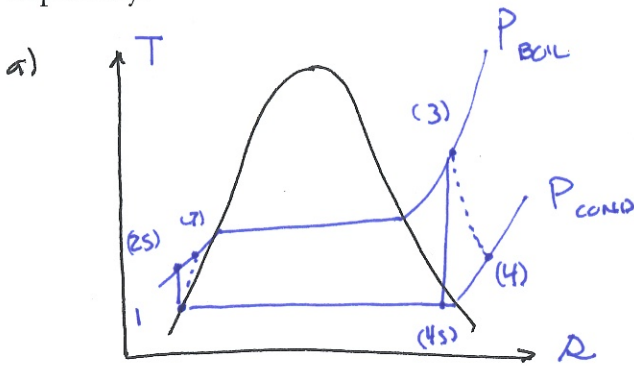
Repeat the last problem, but increase the boiler pressure to 10 MPa.

ANALYSIS AS BEFORE. THESE PROPERTIES CHANGE:

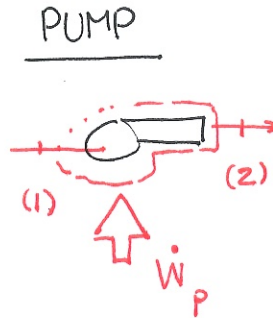
WAS	IS NOW
$h_2 = 1998 \frac{\text{KJ}}{\text{kg}}$	$2018 \frac{\text{KJ}}{\text{kg}}$
$h_3 = 3881 \frac{\text{KJ}}{\text{kg}}$	$3869 \frac{\text{KJ}}{\text{kg}}$
$D_3 = 7.28 \frac{\text{KJ}}{\text{kg} \cdot \text{K}}$	$7.167 \frac{\text{KJ}}{\text{kg} \cdot \text{K}}$
$h_4 = 2307 \frac{\text{KJ}}{\text{kg}}$	$2271 \frac{\text{KJ}}{\text{kg}}$
$W_{P,IN} = 8.058 \frac{\text{KJ}}{\text{kg}}$	$10.07 \frac{\text{KJ}}{\text{kg}}$
$q_{B,IN} = 3682 \frac{\text{KJ}}{\text{kg}}$	$3667 \frac{\text{KJ}}{\text{kg}}$
$W_{T,OUT} = 1575 \frac{\text{KJ}}{\text{kg}}$	$1598 \frac{\text{KJ}}{\text{kg}}$
$q_{C,OUT} = 2115 \frac{\text{KJ}}{\text{kg}}$	$2079 \frac{\text{KJ}}{\text{kg}}$
$\eta_T = 42.6\%$	43.3%
$P_2 = 8 \text{ MPa}$	10 MPa

Example

Repeat the problem again, but this time let the adiabatic efficiencies of the pump and the turbine be 70% and 90%, respectively.



(USE $P_B = 10 \text{ MPa}$)



CONS. OF ENERGY
LOOKS THE SAME,
BUT...

$$\dot{W}_P = \dot{m}(h_2 - h_1)$$

$$w_P = h_2 - h_1 \quad (1)$$

$$h_1 = h(10 \text{ kPa}, x=0) = \checkmark$$

$$h_2 = h(10 \text{ MPa}, \underline{\quad ? \quad}) = ?$$

USE ISENTROPIC EFFICIENCY

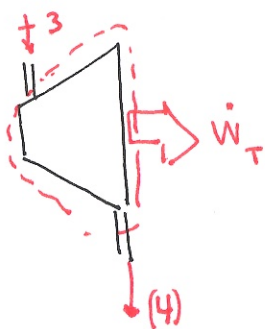
$$\eta_P = \frac{\dot{W}_{IN,P}}{\dot{W}_{IN}} = \frac{w_{IN,P}}{w_{IN}} = \frac{h_{2R} - h_1}{h_2 - h_1}$$

$$\therefore w_P = \frac{w_{IN,S}}{\eta_P} = \frac{h_{2R} - h_1}{\eta_P} = \frac{(201.8 - 191.7) \text{ kJ/kg}}{0.7} = \underline{\underline{14.39 \text{ kJ/kg}}}$$

USE (1) (CONS OF ENERGY) TO FIND h_2 ...

$$h_2 = w_P + h_1 = \dots = 206.1 \text{ kJ/kg}$$

TURBINE IS SIMILAR



$$\dot{W}_T = h_3 - h_4$$

$$w_T = h_3 - h_4$$

$$h_3 = h(10 \text{ MPa}, T=700^\circ\text{C})$$

$$h_4 = h(10 \text{ kPa}, \underline{\quad ? \quad})$$

ISENTROPIC TURBINE EFF. \checkmark ?

$$\eta_T = \frac{w_T}{w_{T,R}} = \frac{h_3 - h_4}{h_3 - h_{4R}}$$

$$W_T = W_{T, \text{in}} \eta_T = (h_3 - h_{4a}) \eta_T$$

$$= (3689 \frac{\text{kJ}}{\text{kg}} - 2271 \frac{\text{kJ}}{\text{kg}}) (0.9) = 1439 \text{ kJ/kg}$$

ANALYSIS of BOILER & COND SAME AS BEFORE. NEW VALUES

$$q_{\text{COND}} = 2239 \text{ kJ/kg} \quad q_{\text{BOIL}} = 3663 \text{ kJ/kg}$$

$$\eta_{\text{TH}} = \frac{W_T - W_P}{q_{\text{BOIL}}} = \frac{(1439 - 14.39) \cancel{\text{kJ/kg}}}{3663 \cancel{\text{kJ/kg}}} = \boxed{0.389}$$

NOTE IT HAS GONE DOWN SIGNIFICANTLY.

FOR POWER PLANTS TO OPERATE WELL, ADIABATIC EFFICIENCIES of TURBINES & PUMPS MUST BE HIGH.