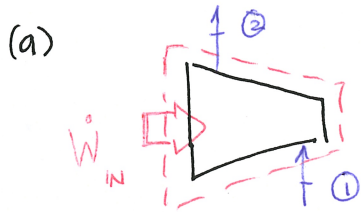
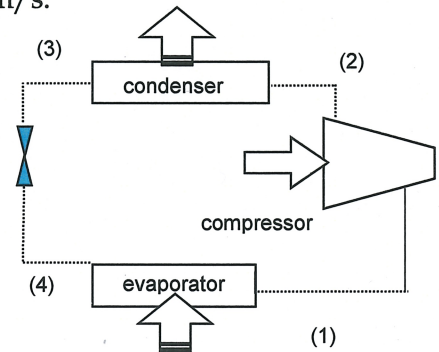


Example

An ideal vapor-compression refrigeration cycle uses R-134a as a working fluid in an air-conditioning system. The refrigerant enters the compressor as a saturated vapor at 40°F and leaves the condenser as a saturated liquid at 130°F. The mass flow rate of the refrigerant is 1.5 lbm/s.

- Find the power into the compressor, in B/s.
- Find the heat transfer rate out of the condenser, in B/s.
- Find the heat transfer rate into the evaporator, in B/s.
- Find the COP for the cycle.
- Find the quality of the refrigerant at the exit of the valve.
- Repeat with an isentropic efficiency for the compressor of $\eta_c=0.85$.



Cons of energy

$$\dot{Q}_0 = \dot{Q}_0 + \dot{W}_{in} + \dot{m}(h_1 + \dots) - \dot{m}(h_2 + \dots)$$

$$\dot{W}_{in} = \dot{m}(h_2 - h_1)$$

$$h_1 = h(T_1, x_1=1) = \underline{108.8 \text{ B/lbm}}$$

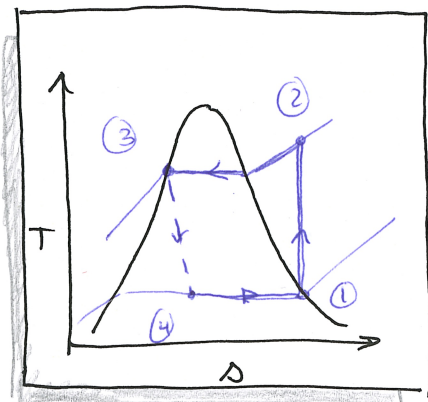
$$P_1 = P(T_1, x_1=1) = \underline{0.2219 \text{ B/(lbm} \cdot \text{R)}}$$

$$h_2 = h(P_2, P_2 = P_1)$$

To find P_2 use state ③

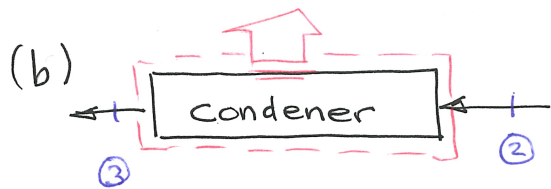
$$P_2 = P_3 = P_{SAT}(T_3) = \underline{213.5 \text{ psia}}$$

$$\therefore h_2 = \underline{121.8 \text{ B/lbm}}$$



T-s diagram

$$\dot{W}_{in} = 1.5 \frac{\text{lb}}{\text{s}} \left((121.8 - 108.8) \frac{\text{B}}{\text{lbm}} \right) = \boxed{19.5 \text{ B/s}}$$



C.O.E. →

$$\dot{L}_0 = -\dot{Q}_{out} + \dot{L}_0 + \dot{m}(h_2 + \dots) - \dot{m}(h_3 + \dots)$$

$$\dot{Q}_{out} = \dot{m}(h_2 - h_3)$$

$$h_3 = h(T_3, x_3 = 0)$$

$$= \underline{56.09 \text{ B/lbm}}$$

$$\dot{Q}_{out} = 1.5 \frac{\text{lbm}}{\text{s}} (121.8 - 56.09) \frac{\text{B}}{\text{lbm}}$$

$$= \boxed{98.6 \text{ B/s}}$$



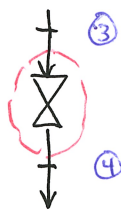
C.O.E. →

$$\dot{L}_0 = \dot{Q}_{in} + \dot{L}_0 + \dot{m}(h_4 + \dots) - \dot{m}(h_1 + \dots)$$

$$\dot{Q}_{in} = \dot{m}(h_1 - h_4)$$

$$h_4 = h(T_4 = T_1, ?)$$

Don't have a second property @ 4 to find h_4 . What to do?



C.O.E. for valve →

$$\dot{L}_0 = \dot{L}_0 + \dot{L}_0 + \dot{m}(h_3 + \dots) - \dot{m}(h_4 + \dots)$$

$$h_4 = h_3 = 56.09 \text{ B/lbm}$$

$$\dot{Q}_{in} = 1.5 \frac{\text{lbm}}{\text{s}} (108.8 - 56.09) \frac{\text{B}}{\text{lbm}}$$

$$= \boxed{79.1 \text{ B/s}}$$



$$(d) \text{ COP}_R = \beta = \frac{\dot{Q}_{in}}{\dot{W}_{in}}$$
$$= \frac{79.1 \text{ Bt/s}}{19.5 \text{ Bt/s}} = \boxed{4.06}$$

$$(e) h_u = (1 - x_u) h_f + x_u h_g$$

$$x_u = \frac{h_u - h_f}{h_g - h_f} = \dots = \boxed{0.372}$$