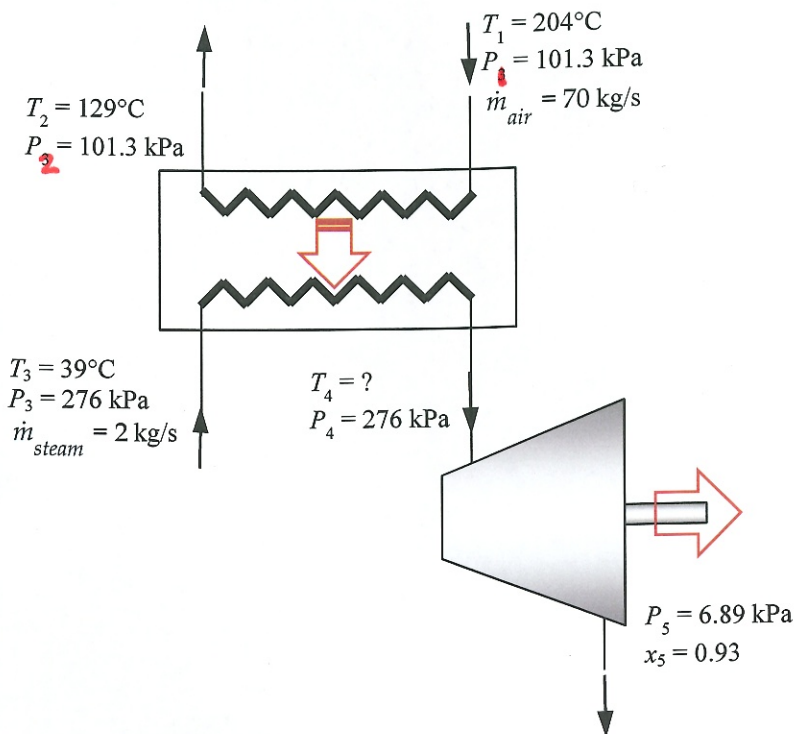


Example

Consider a heat exchanger and a steam turbine used as a waste heat recovery system. The heat exchanger takes hot combustion gases and uses them to heat steam, which in turn passes through a turbine. The gases can be modeled as air treated as an ideal gas with variable specific heats. The surroundings are at $T_0 = 25^\circ\text{C}$ and $P_0 = 101\text{ kPa}$.



- Find the power (in kW) delivered by the turbine.
- Find the isentropic (adiabatic efficiency) of the turbine.
- For the heat recovery system (heat exchanger and turbine combined) identify
 - where inflows of exergy occur

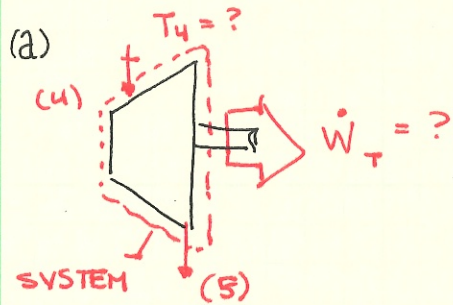
W/AIR IN , W/STEAM IN

- outflows of exergy occur

W/AIR OUT , W/STEAM^{OUT} , W/ \dot{W}_T

- destruction of exergy occur

HXR , IN TURBINE



Cons. of energy →

$$\frac{dE_{sys}}{dt} = \dot{Q}_{in} - \dot{W}_{T,out} + \dot{m}_s(h_4 + \dots) - \dot{m}_s(h_5 + \dots)$$

$$\dot{W}_{T,out} = \dot{m}_s(h_4 - h_5) \quad (1)$$

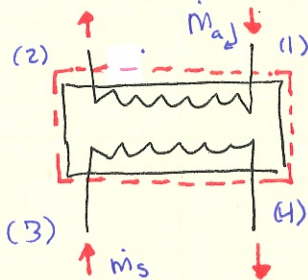
$$h_4 = h(\text{STEAM}, T_4, P_4)$$

$$h_5 = h(\text{STEAM}, P_5, T_5)$$

$$= \underline{2402 \text{ KJ/kg}}$$

NEED h_4 .

Cons of energy on HXR →



$$\dot{Q}_0 = \dot{Q}_0 - \dot{Q}_0 + \sum_{in} \dot{m}(h + \dots) - \sum_{out} \dot{m}(h + \dots)$$

$$0 = \dot{m}_a(h_1) + \dot{m}_s(h_3) - \dot{m}_a(h_2) - \dot{m}_s(h_4)$$

$$h_4 = h_3 + \frac{\dot{m}_a(h_1 - h_2)}{\dot{m}_s}$$

$$h_1 = h(\text{AIR}, T_1)$$

FUNC. of T
ONLY !!

$$= \underline{479.9 \text{ KJ/kg}}$$

$$h_2 = h(\text{AIR}, T_2) = \underline{403.4 \text{ KJ/kg}}$$

$$h_3 = h(\text{STEAM}, T_3, P_3) = \underline{163.6 \text{ KJ/kg}}$$

$$\therefore h_4 = 2838 \text{ KJ/kg} \neq$$

$$\dot{W}_T = 872 \text{ KW}$$

(b)

$$\eta_T = \frac{\dot{W}_{T,out}}{\dot{W}_{T,out,\rho}}$$

$$\dot{W}_{T,out,\rho} = \dot{m}_s(h_4 - h_{5\rho})$$

$$h_{5\rho} = h(\text{STEAM}, P_5, \rho_{5\rho} = \rho_4)$$

$$\rho_4 = \rho(\text{STEAM}, P_4, h_4)$$

$$= 7.291 \text{ KJ/kg-K} \quad !!$$

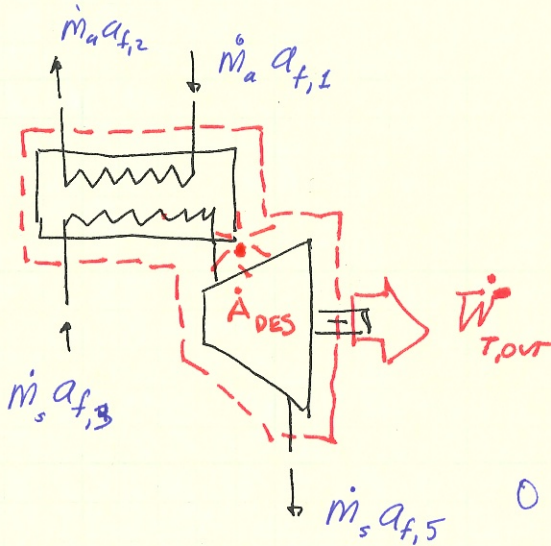
$$\therefore h_{5D} = 2263 \text{ kJ/kg} \rightarrow \dot{W}_{T,P} = 1151 \text{ kW}$$

$$\eta_T = \frac{872 \text{ kW}}{1151 \text{ kW}} = \boxed{0.758}$$

(C) (1) EXERGY IN W/ AIR FLOW, STEAM FLOW
 (2) " " " " " " " "
 & TURBINE POWER

(3) EXERGY DESTRUCTION IN
 • HEAT EXCHANGER (\dot{Q} THRU ΔT)
 • TURBINE ($\eta_T < 1$)

(d)



Acct of A

$$\frac{dA_{sys}}{dt} = \sum_i \left(1 - \frac{T_0}{T_i}\right) \dot{Q}_i - \dot{W}_{out} + \sum_{IN} \dot{m} a_f - \sum_{OUT} \dot{m} a_f - \dot{A}_{DES}$$

$$0 = -\dot{W}_T + \dot{m}_a a_{f,1} + \dot{m}_s a_{f,3} - \dot{m}_a a_{f,2} - \dot{m}_s a_{f,5} - \dot{A}_{DES}$$

$$\dot{A}_{DES} = \underbrace{\dot{m}_a (a_{f,1} - a_{f,2})}_{\text{NET INPUT DUE TO AIR}} - \underbrace{\dot{m}_s (a_{f,5} - a_{f,3})}_{\text{NET OUTFLOW DUE TO STEAM FLOW}} - \underbrace{\dot{W}_T}_{\text{USEFUL OUTPUT}} \quad (2)$$

NET INPUT
DUE TO AIR

NET OUTFLOW
DUE TO STEAM
FLOW

USEFUL OUTPUT

$$a_{f,1} - a_{f,2} = \left\{ h_1 - \cancel{h_{0,air}} - T_0 (\rho_1 - \rho_0) \right\} - \left\{ h_2 - \cancel{h_{0,air}} - T_0 (\rho_2 - \rho_0) \right\}$$

$$= (h_1 - h_2) - T_0 (\rho_1 - \rho_2)$$

$$\rho_1 - \rho_2 = \rho^0(T_1) - \rho^0(T_2) - R \ln \left(\frac{P_2}{P_1} \right)$$

$\rho^0 \neq \rho_0!$ THIS IS A TABLE THING
FOR IDEAL CASES

OR USE FEES:

$$\rho_1 = \rho(\text{AIR}, T_1, P_1) = 6.171 \text{ kJ/kg-K}$$

$$\rho_2 = \rho(\text{AIR}, T_2, P_2) = 5.997 \text{ "}$$

\therefore NET INPUT

$$= \text{NET AIR INPUT} = \dot{m}_a (a_{f,1} - a_{f,2}) = \dots = \underline{1722 \text{ kW}}$$

$$a_{f,5} - a_{f,3} = (h_5 - h_3) - T_0 (\rho_5 - \rho_3)$$

$$h_3 = \checkmark \quad h_5 = \checkmark$$

$$\rho_3 = \rho(\text{STEAM}, T_3, P_3)$$

$$= 0.5588 \text{ kJ/kg-K}$$

$$\rho_5 = \rho(\text{STEAM}, P_5, X_5)$$

$$= 7.739 \text{ kJ/kg-K}$$

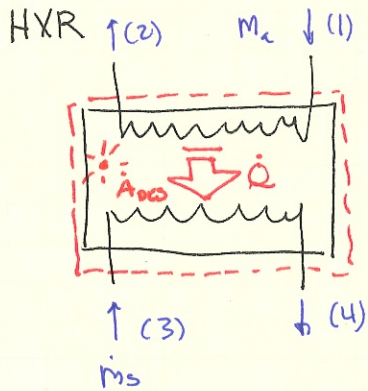
\therefore NET OUTPUT IN STEAM

$$= \dot{m}_s (a_{f,5} - a_{f,3}) = \dots = \underline{199 \text{ kW}}$$

FROM (2)

$$\dot{A}_{DES} = 1722 \text{ kW} - 199 \text{ kW} - 872 \text{ kW} = \underline{651 \text{ kW}}$$

TO KNOW HOW MUCH IS DESTROYED IN HXR & TURBINE,
MUST LOOK @ THOSE AS SEPARATE SYSTEMS.

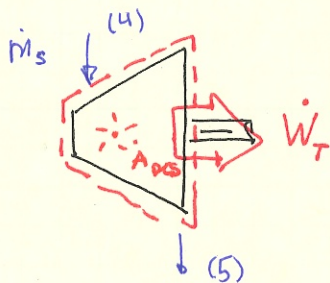


$$\frac{dA_{sys}}{dt} = \sum (1 - \frac{T_o}{T_i}) \dot{Q}_i - \dot{W}_{out} + \sum_{IN} \dot{m} a_f - \sum_{OUT} \dot{m} a_f - \dot{A}_{DES, HXR}$$

$$\dot{A}_{DES, HXR} = \dot{m}_a (a_{f,1}) + \dot{m}_s (a_{f,3}) - \dot{m}_a (a_{f,2}) - \dot{m}_s (a_{f,4})$$

$$\dot{A}_{DES, HXR} = \dot{m}_a (a_{f,1} - a_{f,2}) + \dot{m}_s (a_{f,3} - a_{f,4}) = \dots = \underline{385 \text{ kW}}$$

TURBINE:



$$\frac{dA_{sys}}{dt} = \sum (1 - \frac{T_i}{T_o}) \dot{Q}_i - \dot{W}_{out} + \sum_{IN} \dot{m} a_f - \sum_{OUT} \dot{m} a_f - \dot{A}_{DES, TUR}$$

$$\dot{A}_{DES, TUR} = \dot{m}_s (a_{f,4} - a_{f,5}) - \dot{W}_{T,OUT}$$

$$= \dot{m}_s (h_4 - h_5 - T_o [\Delta_4 - \Delta_5]) - \dot{W}_{T,OUT}$$

$$= \dots = \underline{267 \text{ kW}}$$

FINALLY

NET RATE EXERGY IN
(AIR FLOW)

1722 kW

(100%)

DISPOSITION of EXERGY

• RATE EXERGY OUT

- POWER OUT

872 kW

(50.6%)

- WATER STREAM

199 kW

(11.6%)

• RATE EXERGY DES.

- HXR

385 kW

(22.4%)

- TURBINE

267 kW

(15.5%)

1722 kW

(100%)