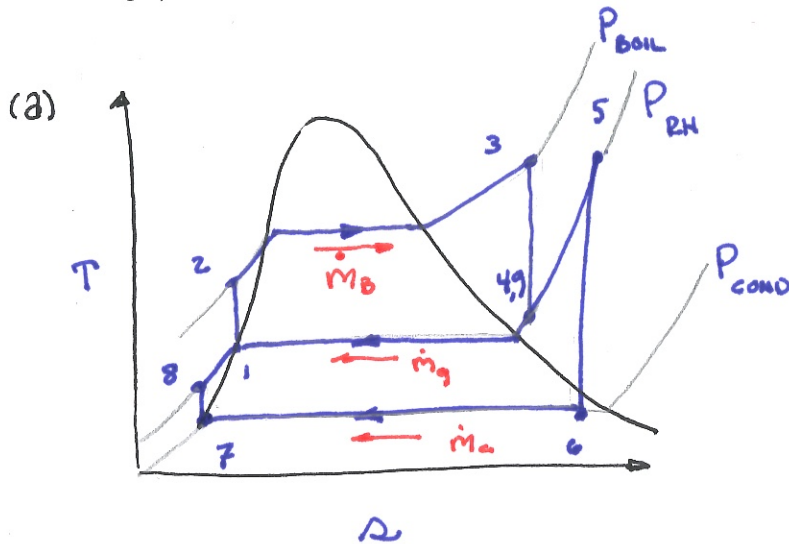
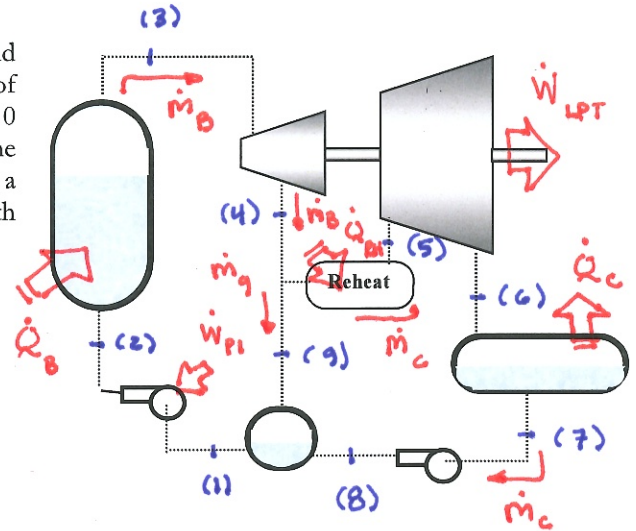


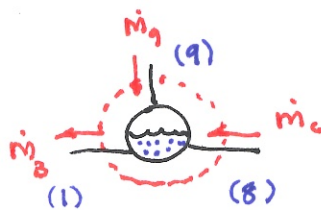
Example

An (almost) ideal Rankine cycle is modified to include reheat and regeneration using an open feedwater heater. The mass flow rate of steam through the boiler is 1.25 kg/s. The boiler operates at 10 MPa, the open feedwater heater operates at 6 MPa, and the condenser operates at 10 kPa. The water enters both pumps as a saturated liquid. The temperature of the steam entering both turbines is 700°C.

- Sketch the cycle on a  $T-s$  diagram.
- Find the power or heat transfer rate in/out of each device. (Hint: Start with an analysis of the open feedwater heater.)
- Find the cycle efficiency. (Hint: Careful with  $\dot{W}_{dot}$  and  $\dot{Q}_{dot}$  vs.  $w_{dot}$  and  $q_{dot}$ .)



(b) OPEN FEEDWATER HEATER



CONS. of MASS

$$\frac{d}{dt}(m_{sys}) = \sum \dot{m}_{in} - \sum \dot{m}_{out}$$

$$0 = \dot{m}_C + \dot{m}_9 - \dot{m}_B \quad (1)$$

CONS. of ENERGY

$$\frac{d}{dt} (E_{\text{SYS}}) = \dot{Q}_{\text{IN,NET}} - \dot{W}_{\text{NET,OUT}} + \sum \dot{m}_i (h + \dots)_{\text{in}} - \sum \dot{m}_e (h + \dots)_{\text{out}}$$

(33)

$$0 = \dot{m}_c (h_8) + \dot{m}_g (h_9) - \dot{m}_B (h_1) \quad (2)$$

$$h_1 = h(P_{RH}, x=0) = \underline{1213 \text{ KJ/kg}}$$

$$h_9 = h(P_{RH}, \Delta = \Delta_3) = \underline{3658 \text{ KJ/kg}}$$

$$\Delta_3 = \Delta(P_{\text{BOIL}}, T = 700^\circ) = \underline{7.167 \text{ KJ/kg}\cdot\text{K}}$$

$$h_8 = h(P_{RH}, \Delta = \Delta_7) = \underline{197.8 \text{ KJ/kg}}$$

$$\Delta_7 = \Delta(P_{\text{COND}}, x=0) = \underline{0.6489 \text{ KJ/kg}\cdot\text{K}}$$

(1) & (2) GIVE  $\dot{m}_c = 0.8831 \text{ kg/s}$

$$\dot{m}_g = 0.3669 \text{ kg/s}$$

CONTINUE W/ CONS. of ENERGY & PROPERTY RELATIONS FOR EACH COMPONENT AROUND CYCLE. RESULTS FOLLOW.

### Given

$$P_{\text{cond}} = 10 \text{ [kPa]}$$

$$P_{\text{boil}} = 10000 \text{ [kPa]}$$

$$P_{\text{reheat}} = 6000 \text{ [kPa]}$$

$$T_3 = 700$$

$$\dot{m}_B = 1.25 \text{ [kg/s]}$$

### Pump 1 energy

$$\dot{W}_{p,1} = \dot{m}_B \cdot [h_2 - h_1]$$

$$h_1 = \mathbf{h} \text{ ['Steam', } P = P_{\text{reheat}}, x = 0 \text{ ]}$$

$$s_1 = \mathbf{s} \text{ ['Steam', } P = P_{\text{reheat}}, x = 0 \text{ ]}$$

$$h_2 = \mathbf{h} \text{ ['Steam', } P = P_{\text{boil}}, s = s_1 \text{ ]}$$

### Boiler energy

$$\dot{Q}_B = \dot{m}_B \cdot [h_3 - h_2]$$

$$h_3 = \mathbf{h} \text{ ['Steam', } T = T_3, P = P_{\text{boil}} \text{ ]}$$

$$s_3 = \mathbf{s} \text{ ['Steam', } T = T_3, P = P_{\text{boil}} \text{ ]}$$

### HP Turbine energy

$$\dot{W}_{\text{HPT}} = \dot{m}_B \cdot [h_3 - h_4]$$

$$h_4 = \mathbf{h} \text{ ['Steam', } P = P_{\text{reheat}}, s = s_3 \text{ ]}$$

### Reheater energy

$$\dot{Q}_{\text{reheat}} = \dot{m}_C \cdot [h_5 - h_4]$$

$$h_5 = \mathbf{h} \text{ ['Steam', } T = T_3, P = P_{\text{reheat}} \text{ ]}$$

### LP turbine energy

$$\dot{W}_{\text{LPT}} = \dot{m}_C \cdot [h_5 - h_6]$$

$$s_5 = \mathbf{s} \text{ ['Steam', } T = T_3, P = P_{\text{reheat}} \text{ ]}$$

$$h_6 = \mathbf{h} \text{ ['Steam', } P = P_{\text{cond}}, s = s_5 \text{ ]}$$

### Condensor energy

$$\dot{Q}_C = \dot{m}_C \cdot [h_6 - h_7]$$

$$h_7 = \mathbf{h} \text{ ['Steam', } P = P_{\text{cond}}, x = 0 \text{ ]}$$

### Pump 2 energy

$$\dot{W}_{p,2} = \dot{m}_C \cdot [h_8 - h_7]$$

$$s_7 = \mathbf{s} [\text{'Steam'}, P = P_{\text{cond}}, x = 0]$$

$$h_8 = \mathbf{h} [\text{'Steam'}, P = P_{\text{reheat}}, s = s_7]$$

*Open feedwater heater*

*Mass*

$$0 = \dot{m}_C + \dot{m}_9 - \dot{m}_B$$

*Energy*

$$0 = \dot{m}_9 \cdot h_4 + \dot{m}_C \cdot h_8 - \dot{m}_B \cdot h_1$$

*Cycle efficiency. Notice that we use power and rate of heat transfer (big W and Q, not little w and q) because the mass flow rates are different through different components.*

$$\eta = \frac{\dot{W}_{\text{HPT}} + \dot{W}_{\text{LPT}} - \dot{W}_{p,1} - \dot{W}_{p,2}}{\dot{Q}_B + \dot{Q}_{\text{reheat}}}$$

SOLUTION

**Unit Settings: SI C kPa kJ mass deg**

$$\eta = 0.4581$$

$$h_2 = 1219 \text{ [kJ/kg]}$$

$$h_4 = 3658 \text{ [kJ/kg]}$$

$$h_6 = 2352 \text{ [kJ/kg]}$$

$$h_8 = 197.9 \text{ [kJ/kg]}$$

$$\dot{m}_B = 1.25 \text{ [kg/s]}$$

$$P_{\text{boil}} = 10000 \text{ [kPa]}$$

$$P_{\text{reheat}} = 6000 \text{ [kPa]}$$

$$\dot{Q}_C = 1908 \text{ [kW]}$$

$$s_1 = 3.027 \text{ [kJ/kg-K]}$$

$$s_5 = 7.423 \text{ [kJ/kg-K]}$$

$$T_3 = 700 \text{ [C]}$$

$$\dot{W}_{\text{LPT}} = 1361 \text{ [kW]}$$

$$\dot{W}_{p,2} = 5.338 \text{ [kW]}$$

$$h_1 = 1213 \text{ [kJ/kg]}$$

$$h_3 = 3869 \text{ [kJ/kg]}$$

$$h_5 = 3894 \text{ [kJ/kg]}$$

$$h_7 = 191.8 \text{ [kJ/kg]}$$

$$\dot{m}_9 = 0.3669 \text{ [kg/s]}$$

$$\dot{m}_C = 0.8831 \text{ [kg/s]}$$

$$P_{\text{cond}} = 10 \text{ [kPa]}$$

$$\dot{Q}_B = 3313 \text{ [kW]}$$

$$\dot{Q}_{\text{reheat}} = 208.2 \text{ [kW]}$$

$$s_3 = 7.167 \text{ [kJ/kg-K]}$$

$$s_7 = 0.6493 \text{ [kJ/kg-K]}$$

$$\dot{W}_{\text{HPT}} = 263.9 \text{ [kW]}$$

$$\dot{W}_{p,1} = 6.579 \text{ [kW]}$$

No unit problems were detected.