

**Example**

Acetylene ( $C_2H_2$ ) at a fuel flow rate of 1 kg/min is burned with dry air with an air fuel ratio of 17:1. Assuming **complete combustion** and a total pressure of 110 kPa, find

- the percent excess air used,
- the **equivalence ratio**,
- the percentage of  $CO_2$  in the products by volume,
- the dew point temperature of the products in  $^{\circ}C$ ,
- the percentage of water vapor condensed if the products are cooled to  $20^{\circ}C$ , and
- the required volume flow rate of dry air if it is supplied at  $22^{\circ}C$  and 110 kPa.
- If the actual air supplied has a humidity ratio of 16 g  $H_2O$  per kg of dry air, find the dew point temperature of the products.

(2) COMPARE TO STOICH:



$$C: 2\cancel{c} = b\cancel{c} \quad b=2$$

$$H: 2 = 2c \quad c=1$$

$$O: 2a = 2b + c \quad 2a = 2 \cdot 2 + 1 \quad a = 2.5$$

$$N_2: (\cancel{2})(3.76) a = \cancel{2}d \quad d = 3.76(a) = 3.76(2.5)$$

$$d = 9.4$$



THEORETICAL RXN

$$AF_{ACT} = 17 = \frac{m_{air}}{m_{fuel}} = \frac{n_{air} M_{air}}{n_{fuel} M_{fuel}} = \frac{n_a}{n_f} \frac{29 \text{ kg/kmol}}{26.04 \text{ kg/kmol}} \Rightarrow$$

$$(n_a/n_f) = 15.26$$

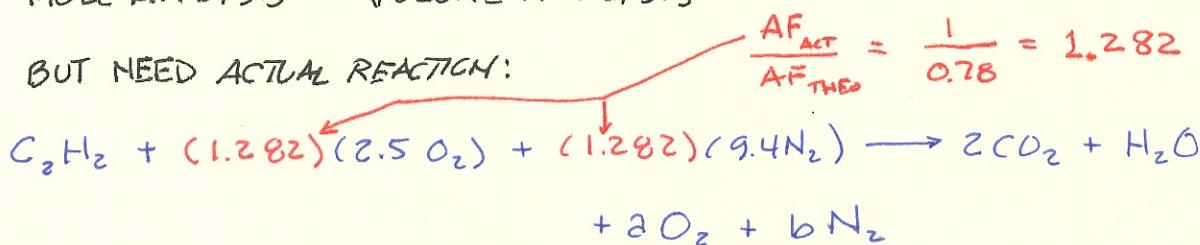
$$(n_a/n_{f, \text{theo.}}) = 2.5 \underbrace{(O_2 + 3.76 N_2)}_{4.76 \text{ mol air}} = 11.9$$

$$\therefore \% \text{ EXCESS} = \frac{15.26 - 11.9}{11.9} * 100 = \boxed{28.2\%}$$

$$(b) \phi = \frac{F_{A_{ACT}}}{F_{A_{THEO}}} = \frac{\frac{1}{17}}{\frac{n_f M_f}{n_a M_a}} = \frac{\frac{1}{17}}{\frac{1}{11.9} \frac{26.04}{29}} = \boxed{0.78}$$

(c) MOLE ANALYSIS  $\rightarrow$  VOLUME ANALYSIS

BUT NEED ACTUAL REACTION:



$$O_2: (1.282)(2.5)(2) = (2)(2) + 1 + 2a$$

$$a = 0.705$$

$$N: (1.282)(9.4)(2) = 2b \quad b = 12.05$$

BALANCED ACTUAL RXN:



$$\% CO_{PROT} = \frac{2}{2+1+12.05+0.705} \times 100 = \boxed{12.7\%}$$

$$(d) T_{DEW} = T_{SAT}(P_v)$$

$$P_v = y_v P \quad y_v = \frac{1}{2+1+12.05+0.705} = \underline{0.0635}$$

$$P_v = (0.0635)(110 \text{ kPa}) = 6.98 \text{ kPa}$$

$$T_{DEW} = T_{SAT}(6.98 \text{ kPa}) = \boxed{38.8^\circ C}$$

COULD YOU HAVE USED PSYCH. CHART? NO!  $P_{TOTAL} \neq 101.325 \text{ kPa}$ !(e)  $20^\circ C < T_{DEW} \Rightarrow$  WATER WILL CONDENSE.

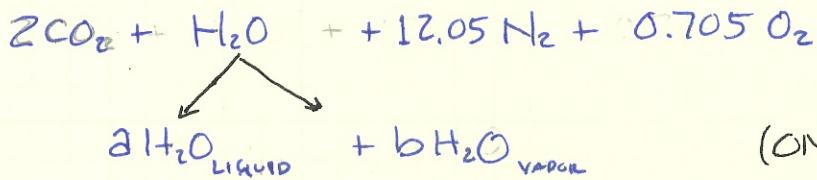
$$\rightarrow \text{PRDTS ARE SATURATED} \Rightarrow P_{v, PROT} = P_{SAT}(20^\circ C) \\ = 2.339 \text{ kPa}$$

$$y_v P = P_v \Rightarrow y_v = \frac{P_v}{P}$$

$$= \frac{2.339 \text{ kPa}}{110 \text{ kPa}} = 0.02126$$

$$\% \text{ CONDENSE} = \frac{N_{H_2O, \text{LIQUID}}}{N_{H_2O, \text{TOTAL}}} = \frac{N_{H_2O, \text{LIQUID}}}{N_{H_2O, \text{VAP}} + N_{H_2O, \text{LIQUID}}} \times 100\%$$

LOOK @ PR DTS:



(ONLY VAPOR of  $H_2O$

CONTRIBUTES TO  $y_v$ .)

$$y_v = \frac{b}{2 + b + 12.05 + 0.705}$$

$$= 0.02126 \Rightarrow b = 0.321$$

$$\therefore \alpha = 1 - b = 0.679 \quad \% \text{ COND} = \frac{0.679}{1} \times 100\% = 67.9\%$$

(f)

$$\dot{V} = \dot{m}_{\text{air}} v_a$$

$$\dot{m}_{\text{air}} = (\text{AF}) \dot{m}_{\text{fuel}}$$

$$= (17)(1 \text{ kg/s}) = 17 \text{ kg/s min}$$

$$v_a = \frac{R_a T}{P_a}$$

$$= \frac{(0.287 \text{ kJ/kg.K})(22 + 273) \text{ K}}{110 \text{ kPa}} = \frac{0.770 \text{ m}^3/\text{kg}}{\text{kg}}$$

$$\dot{V} = (17 \text{ kg/min}) (0.770 \text{ m}^3/\text{kg}) = 13.1 \text{ m}^3/\text{min}$$

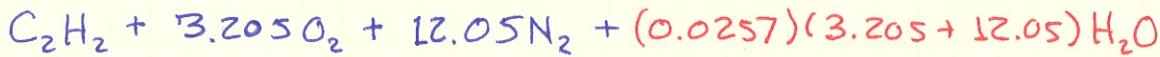
(g) NEED A NEW RXN! AGAIN!

$$\omega_{\text{RT}} = 0.0016 \frac{\text{kg V}}{\text{kg air}} = \frac{M_{H_2O}}{M_{\text{air}}} = \frac{N_{H_2O} M_{H_2O}}{N_{\text{air}} M_{\text{air}}} = 0.622 \frac{N_{H_2O}}{N_{\text{air}}}$$

$$\therefore N_{H_2O, \text{ext}} = \frac{(0.0016)}{(0.622)} N_{\text{air}} = 0.0257 N_{\text{air}}$$

LOOK  
FAMILIAR?

NEW RXN:



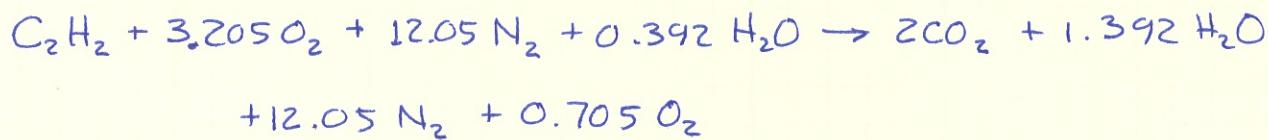
$$H: (0.0257)(3.205 + 12.05)(2) = (2)(2)$$

$$2 = 1.392$$

$$O: 3.205(2) + (0.0257)(3.205 + 12.05) = (2)(2) + \check{a} + b(2)$$

$$\dots b = 0.705 \leftarrow \text{UNCHANGED. WHY?}$$

BALANCED RXN:



$$y_{v_{\text{prod}}} = \frac{1.392}{2 + 1.392 + 12.05 + 0.705} = 0.0862$$

$$P_{v_{\text{prod}}} = y_{v_{\text{prod}}} P = (0.0862)(110 \text{ kPa}) = 9.483 \text{ kPa}$$

$$T_{\text{DEW}} = T_{\text{sat}}(9.483 \text{ kPa}) = \boxed{44.7^\circ C}$$