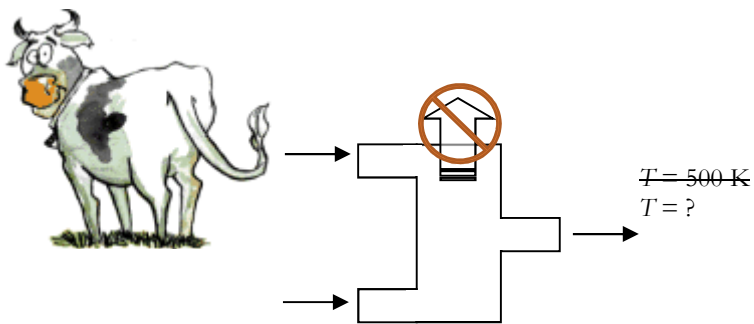


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**EXAMPLE: Open system mixing**

Let us reconsider the dubious bovine flatulence energy source problem yet again. As before, the proposed process combusts methane ( $\text{CH}_4$ ) with air in a steady-state reaction chamber and produces 90%  $\text{CO}_2$ , 10%  $\text{CO}$  and no  $\text{O}_2$  in the products. Both the methane and the air enter at 1 bar and  $25^\circ\text{C}$ .

This time, however, we will *not* assume that the products leave the chamber at 500 K and 1 bar. Rather, we will assume the chamber operates *adiabatically* and at constant pressure. You are to find the exit temperature of the products. That is, you are to find the



| $i$                     | $T$<br>[K] | $\Delta \bar{h}_f^0$<br>[kJ/kmol] | $\bar{h}(T)$<br>[kJ/kmol] | $\bar{h}(298\text{K})$<br>[kJ/kmol] | $\bar{h}$<br>[kJ/kmol] |
|-------------------------|------------|-----------------------------------|---------------------------|-------------------------------------|------------------------|
| $\text{CO}_2)_2$        |            |                                   |                           |                                     |                        |
| $\text{CO})_2$          |            |                                   |                           |                                     |                        |
| $\text{H}_2\text{O})_2$ |            |                                   |                           |                                     |                        |
| $\text{N}_2)_2$         |            |                                   |                           |                                     |                        |
| $\text{CH}_4)_1$        |            |                                   |                           |                                     |                        |
| $\text{O}_2)_1$         |            |                                   |                           |                                     |                        |
| $\text{N}_2)_1$         |            |                                   |                           |                                     |                        |