

CONSERVATION of MASS

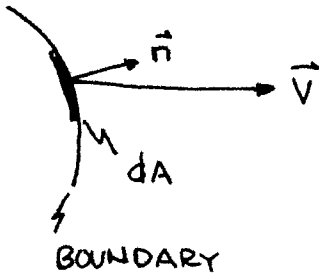
GENERAL RATE EQN:

$$\frac{dm_{sys}}{dt} = \sum \dot{m}_{in} - \sum \dot{m}_{out}$$

WHERE

$$m_{sys} = \int_{V_{sys}} \rho dV$$

MASS FLOW CALCULATIONS



$$\dot{m} = \int_A \rho \vec{V} \cdot \vec{n} dA = \int_A \rho V_n dA$$

- IF $\rho = \text{CONST}$ (INCOMPRESS. APPROX. \rightarrow MOST LIQUIDS & SOLIDS)

$$\dot{m} = \rho \int_A V_n dA = \rho \dot{V}$$

VOLUMETRIC
FLOW
RATE

- IF ρ IS CONST & V IS UNIFORM

$$\dot{m} = \rho V_n A$$

- IF ρ IS CONST & V IS NOT UNIFORM

$$\dot{m} = \rho V_{n,AVG} A \quad \text{DEFINES } V_{AVG}$$

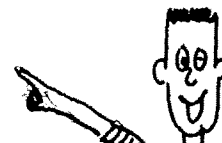
FINITE TIME FORM of MASS CONS.:

$$m_{sys}(t_2) - m_{sys}(t_1) = \sum \dot{m}_{in} - \sum \dot{m}_{out}$$



BY INTEGRATING RATE FORM

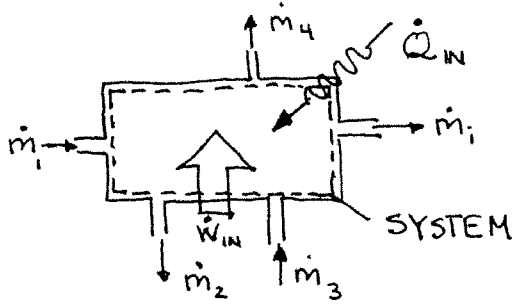
I CAN DO
THAT
WITHOUT
MAPLE!



CONSERVATION of ENERGY

(SUMMARY)

The "Big, Naggy Equation":



$$\frac{dE_{sys}}{dt} = \underbrace{\dot{Q}_{IN} + \dot{W}_{IN}}_{\text{NON-FLOW BOUNDARIES}} + \underbrace{\sum_{IN} \dot{m} \left(h + \frac{V^2}{2} + gz \right) - \sum_{OUT} \dot{m} \left(h + \frac{V^2}{2} + gz \right)}_{\text{FLOW BOUNDARIES}}$$

• $E_{sys} = E_{KE} + E_{PE} + U + \dots E_{sp} \text{ (MAYBE) } \dots$

$E_{KE} = \frac{1}{2} m_{sys} V_{sys}^2$

$E_{PE} = m_{sys} g z_{sys}$

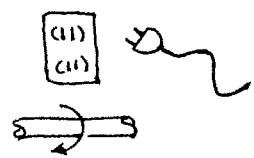
$U = \text{Internal Energy} = m_{sys} u_{sys}$

specific internal energy

• \dot{Q}_{IN} = RATE of HEAT TRANSFER IN. (DUE TO A TEMPERATURE DIFFERENCE.)

• \dot{W}_{IN} = POWER IN @ Non-flow boundaries.

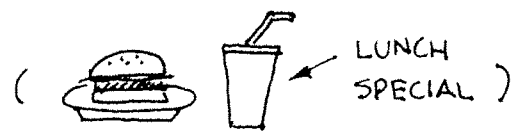
- CAN BE ELECTRICAL $\dot{W}_{ELEC} = i(V_A - V_B)$
- " " SHAFT PWR $\dot{W}_{SHFT} = \vec{\tau} \cdot \vec{\omega}$
- " " SHEAR/FRICTION $\dot{W}_F = \vec{F}_F \cdot \vec{V}$
 $= (\mu N) \hat{e}_p \cdot \vec{V}$



• $h \equiv u + pv$
 $\equiv u + p/g$
 = SPECIFIC ENTHALPY

SPECIAL FORMS (DON'T MEMORIZE - DERIVE!)

CLOSED SYS	CLOSED SYS, FINITE TIME
$\frac{dE_{sys}}{dt} = \dot{Q}_{IN} + \dot{W}_{IN}$	$E_{sys,2} - E_{sys,1} = Q_{IN} + W_{IN}$



COMMON MISTAKES

AND

HOW TO AVOID THEM

DOES $\dot{w} = -\int p dV$?

NO! $w = -\int p dV$, \neq THAT'S JUST COMP/EXP WORK. DON'T BE SLOPPY W/ YOUR DOTS. YES DOT \rightarrow POWER; NO DOT \rightarrow WORK.

I DON'T KNOW WHEN TO USE h \neq WHEN TO USE u .

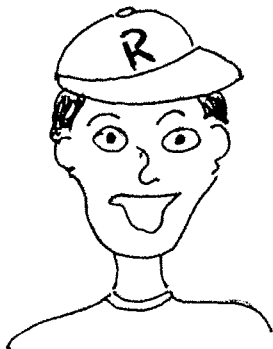
CLEARLY DEFINE YOUR SYSTEM \neq TIME FRAME. Usually (NOT ALWAYS) u POPS UP IN CLOSED SYSTEMS \neq h IN OPEN SYSTEMS.

I DON'T KNOW WHEN TO IGNORE K.E. \neq P.E.

EXPERIENCE WILL GUIDE YOU (SO DO MORE PROBLEMS!) IF YOU HAVE K.E. \neq P.E. INFO, INCLUDE IT \neq SEE IF IT'S SIGNIFICANT.

I KEEP MESSING UP THE SIGN ON Q AND w .

WRITE Q, \dot{w} , ETC. W/ IN/OUT SUBSCRIPTS; E.G., w_{IN} , \dot{Q}_{OUT} .



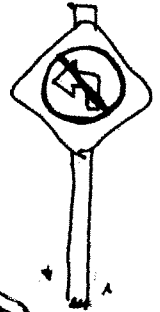
ASK DR. THOM!



ENTROPY & THE 2ND LAW OF THERMO



ALL REAL PROCESSES HAVE PREFERRED DIRECTIONS. THIS IS ONE STATEMENT OF THE SECOND LAW OF THERMO...



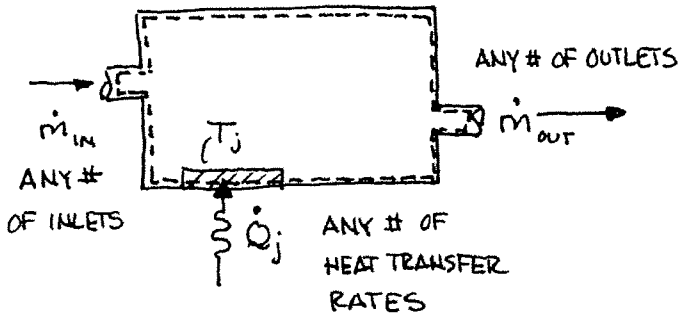
ANOTHER STATEMENT IS THAT **ENTROPY** (AN EXTENSIVE PROPERTY) CAN ONLY BE PRODUCED. IN THE LIMIT OF AN INTERNALLY REVERSIBLE PROCESS, ENTROPY IS CONSERVED.

IN EQN FORM \Rightarrow (ENTROPY ACCOUNTING)

$$\frac{dS_{sys}}{dt} = \sum \frac{\dot{Q}_j}{T_j} + \underbrace{\sum_{IN} \dot{m} \alpha - \sum_{OUT} \dot{m} \alpha}_{\text{Net rate of transport of entropy due to mass flow}} + \dot{S}_{GEN}$$

\uparrow Rate of change of entropy of system
 \uparrow Rate of entropy transport in due to \dot{Q}
 Net rate of transport of entropy due to mass flow
 \uparrow Entropy generation

$\dot{S}_{GEN} > 0$ IF INTERNALLY IRREVERSIBLE
 $\dot{S}_{GEN} = 0$ IF INTERNALLY REVERSIBLE

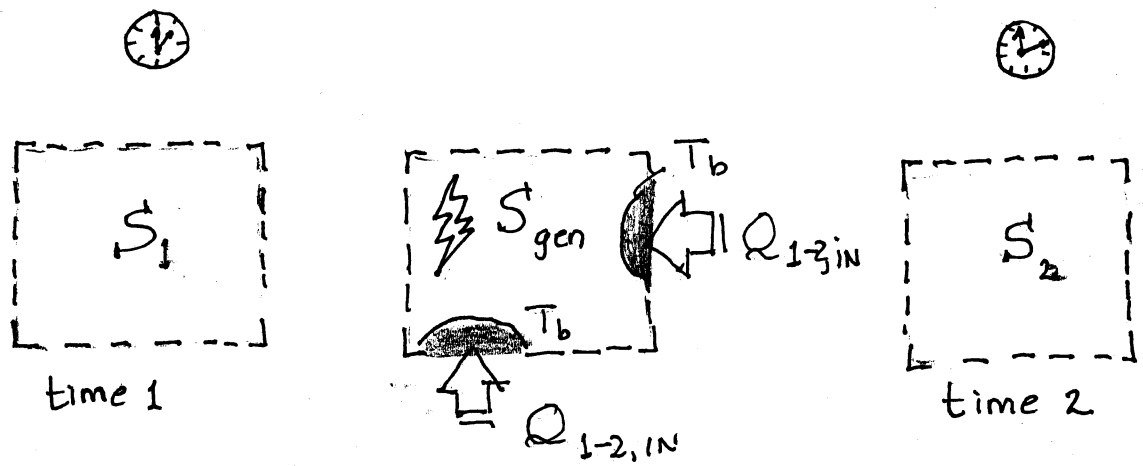


T_j IS ABSOLUTE TEMPERATURE OF SYSTEM BOUNDARY WHERE \dot{Q} CROSSES.

- DIMENSIONS of S : [ENERGY] [TEMP.]
- α : ENTROPY PER UNIT MASS



CLOSED SYSTEM, FINITE TIME



$$(S_2 - S_1)_{SYSTEM} = \sum_i \frac{Q_{IN,1 \rightarrow 2}}{T_{b,i}} + S_{gen}$$

Increase in system S from time 1 to time 2

Transport of S into system with Q

S generated inside system during time 1 to time 2

CLOSED