
 Name

**ME301 – Applications of
 Thermodynamics**

 Circle section: 01 [6th Cloutier] 02 [5th Thom]
 03 [6th Thom] 04 [5th Lui]
 05 [6th Lui]

Exam 2

Oct 25, 2018

Rules:

- Closed book/notes exam.
- Two help sheets allowed. (8-1/2 x 11" sheet of paper, one side each, handwritten; may not contain worked out example problems)
- Maple, Excel, and MATLAB are allowed on your laptop, but nothing may be prepared before the exam.
- Either open property tables (hardcopies) or open Property Calculator Programs on your laptop.

Instructions:

- Show all work for complete credit.
- Work in symbols first, plugging in numbers and performing calculations last.

Problem 1	_____ / 24
Problem 2	_____ / 32
Problem 3	_____ / 44
Total	_____ / 100

Problem 1 [24 points]

(a) [6 pts] Two steam turbines with isentropic (adiabatic) efficiencies of $\eta_A = 1$ and $\eta_B = 0.85$ are considered for use in the same Rankine cycle. How would the various quantities compare for the two turbines?

i. Outlet specific entropies of the turbines

- $s_{out,B} < s_{out,A}$
- $s_{out,B} = s_{out,A}$
- $s_{out,B} > s_{out,A}$

ii. Outlet specific enthalpies of the turbines

- $h_{out,B} < h_{out,A}$
- $h_{out,B} = h_{out,A}$
- $h_{out,B} > h_{out,A}$

iii. Outlet pressures of the turbines

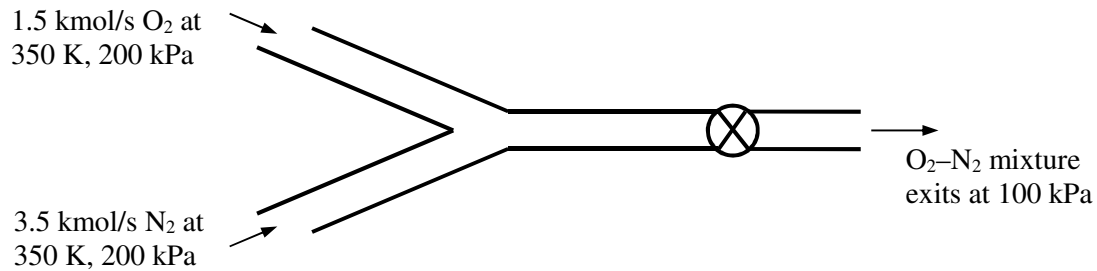
- $P_{out,B} < P_{out,A}$
- $P_{out,B} = P_{out,A}$
- $P_{out,B} > P_{out,A}$

(b) [12 pts] A mixture of fuel and oxygen is modeled as having the following molar composition: 34% CH_4 ($M_{\text{CH}_4}=16.04$) and 66% O_2 ($M_{\text{O}_2}=32$). Find the mass fraction of each component and the apparent (average) molar mass of the mixture.

- (c) [6 pts] In a *cold air standard* Brayton cycle, the exit temperature of the air leaving the turbine is $T_4=200^\circ\text{C}$ and the temperature of the air leaving the compressor is $T_2=100^\circ\text{C}$.
- i. If the cycle makes use of an ideal regenerator, the temperature of the air entering the high pressure heat exchanger will be
 - $T_x = 100^\circ\text{C}$
 - $100^\circ\text{C} < T_x < 200^\circ\text{C}$
 - $T_x = 200^\circ\text{C}$
 - ii. If the cycle makes use of a non-ideal regenerator, the temperature of the air entering the high pressure heat exchanger will be
 - $T_x = 100^\circ\text{C}$
 - $100^\circ\text{C} < T_x < 200^\circ\text{C}$
 - $T_x = 200^\circ\text{C}$
 - iii. If the cycle is instead an *air-standard* Brayton cycle (not cold air standard), ideal regeneration would result in
 - $T_x = 100^\circ\text{C}$
 - $100^\circ\text{C} < T_x < 200^\circ\text{C}$
 - $T_x = 200^\circ\text{C}$

Problem 2 [32 points]

1.5 kmol/s of gaseous oxygen at 350 K and 200 kPa is mixed with 3.5 kmol/s of gaseous nitrogen at 350 K and 200 kPa. The mixture stream is then throttled to standard room pressure at 100 kPa through a valve.

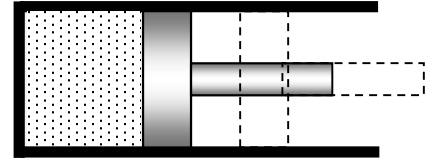


- (a) If the process is *adiabatic*, determine the mixture temperature at the exit.
- (b) Determine the entropy generation rate during the mixing-throttling process, in kW/K.

Clearly document your solution for full credit.

Problem 3 [44 points]

A piston-cylinder operates on the Worst-Efficiency-Ever Cycle (WEEC) with steam as the working fluid. The cycle consists of the following three processes:

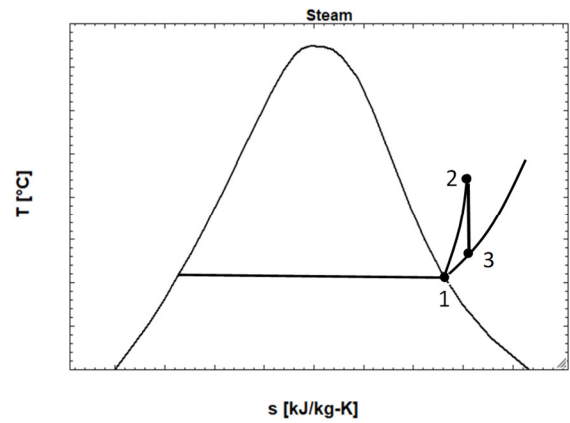
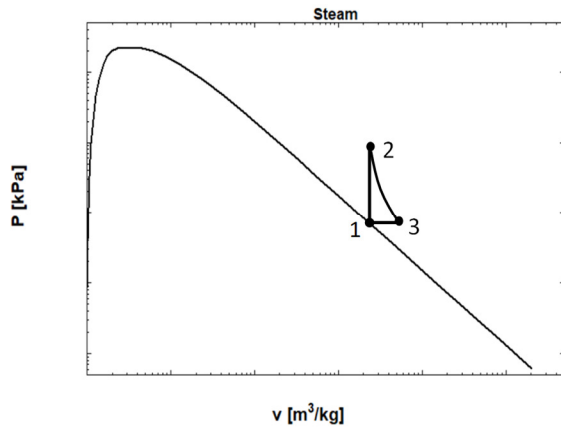


- State (1) to (2): Constant volume heat addition
- State (2) to (3): Reversible, adiabatic expansion
- State (3) to (1): Constant pressure heat rejection

At the beginning of the heat addition process, 0.1 kg of water exists as a saturated vapor at 100 kPa.

Process	W (kJ)	Q (kJ)
(1) → (2)		27.29
(2) → (3)		
(3) → (1)		

- (a) Find the maximum cycle temperature.
- (b) Fill in the table with the work and heat transfer associated with each requested process. (**Note: show all work for full credit.**)
- (c) Calculate the cycle efficiency.



Length

$$1 \text{ ft} = 12 \text{ in} = 0.3048 \text{ m} = 1/3 \text{ yd}$$

$$1 \text{ m} = 100 \text{ cm} = 1000 \text{ mm} = 39.37 \text{ in} = 3.2808 \text{ ft}$$

$$1 \text{ mile} = 5280 \text{ ft} = 1609.3 \text{ m}$$

Mass

$$1 \text{ kg} = 1000 \text{ g} = 2.2046 \text{ lbm}$$

$$1 \text{ lbm} = 16 \text{ oz} = 0.45359 \text{ kg}$$

$$1 \text{ slug} = 32.174 \text{ lbm}$$

Temperature Values

$$(T/\text{K}) = (T/^\circ\text{R}) / 1.8$$

$$(T/\text{K}) = (T/^\circ\text{C}) + 273.15$$

$$(T/^\circ\text{C}) = [(T/^\circ\text{F}) - 32] / 1.8$$

$$(T/^\circ\text{R}) = 1.8(T/\text{K})$$

$$(T/^\circ\text{R}) = (T/^\circ\text{F}) + 459.67$$

$$(T/^\circ\text{F}) = 1.8(T/^\circ\text{C}) + 32$$

Temperature Differences

$$(\Delta T/^\circ\text{R}) = 1.8(\Delta T/\text{K})$$

$$(\Delta T/^\circ\text{R}) = (\Delta T/^\circ\text{F})$$

$$(\Delta T/\text{K}) = (\Delta T/^\circ\text{C})$$

Volume

$$1 \text{ m}^3 = 1000 \text{ L} = 10^6 \text{ cm}^3 = 10^6 \text{ mL} = 35.315 \text{ ft}^3$$

$$= 264.17 \text{ gal}$$

$$1 \text{ ft}^3 = 1728 \text{ in}^3 = 7.4805 \text{ gal} = 0.028317 \text{ m}^3$$

$$1 \text{ gal} = 0.13368 \text{ ft}^3 = 0.0037854 \text{ m}^3$$

Volumetric Flow Rate

$$1 \text{ m}^3/\text{s} = 35.315 \text{ ft}^3/\text{s} = 264.17 \text{ gal}/\text{s}$$

$$1 \text{ ft}^3/\text{s} = 1.6990 \text{ m}^3/\text{min} = 7.4805 \text{ gal}/\text{s}$$

$$= 448.83 \text{ gal}/\text{min}$$

Force

$$1 \text{ N} = 1 \text{ kg m}/\text{s}^2 = 0.22481 \text{ lbf}$$

$$1 \text{ lbf} = 1 \text{ slug ft}/\text{s}^2 = 32.174 \text{ lbm ft}/\text{s}^2$$

$$= 4.4482 \text{ N}$$

Pressure

$$1 \text{ atm} = 101.325 \text{ kPa} = 1.01325 \text{ bar}$$

$$= 14.696 \text{ lbf}/\text{in}^2$$

$$1 \text{ bar} = 100 \text{ kPa} = 10^5 \text{ Pa}$$

$$1 \text{ Pa} = 1 \text{ N}/\text{m}^2 = 10^{-3} \text{ kPa}$$

$$1 \text{ lbf}/\text{in}^2 = 6.8947 \text{ kPa} = 6894.7 \text{ N}/\text{m}^2 ;$$

$$[\text{lbf}/\text{in}^2 = \text{“psi”}]$$

Energy

$$1 \text{ J} = 1 \text{ N m}$$

$$1 \text{ J} = 1 \text{ Pa m}^3$$

$$1 \text{ kJ} = 1000 \text{ J} = 737.56 \text{ ft} \cdot \text{lbf} = 0.94782 \text{ Btu}$$

$$1 \text{ Btu} = 1.0551 \text{ kJ} = 778.17 \text{ ft} \cdot \text{lbf}$$

$$1 \text{ ft} \cdot \text{lbf} = 1.3558 \text{ J}$$

Energy Transfer Rate

$$1 \text{ kW} = 1 \text{ kJ}/\text{s} = 737.56 \text{ ft} \cdot \text{lbf}/\text{s} = 1.3410$$

$$\text{hp} = 0.94782 \text{ Btu}/\text{s}$$

$$1 \text{ Btu}/\text{s} = 1.0551 \text{ kW} = 1.4149 \text{ hp}$$

$$= 778.17 \text{ ft} \cdot \text{lbf}/\text{s}$$

$$1 \text{ hp} = 550 \text{ ft} \cdot \text{lbf}/\text{s} = 0.74571 \text{ kW}$$

$$= 0.70679 \text{ Btu}/\text{s}$$

Specific Energy

$$1 \text{ kJ}/\text{kg} = 1000 \text{ m}^2/\text{s}^2$$

$$1 \text{ Btu}/\text{lbm} = 25037 \text{ ft}^2/\text{s}^2$$

$$1 \text{ ft} \cdot \text{lbf} / \text{lbm} = 32.174 \text{ ft}^2/\text{s}^2$$

Other useful information	SI	USCS
Universal Ideal Gas Constant: \bar{R}	$= 8.314 \text{ kJ}/(\text{kmol} \cdot \text{K})$	$= 1545 \text{ (ft} \cdot \text{lbf)} / (\text{lbmol} \cdot \text{R})$ $= 1.986 \text{ Btu}/(\text{lbmol} \cdot \text{R})$
Acceleration of Gravity: g	$= 9.810 \text{ m}/\text{s}^2$	$= 32.174 \text{ ft}/\text{s}^2$