NAME $\qquad$ Campus Mailbox $\qquad$
INSTRUCTOR (Circle One):

Cunningham (5th Period) Livesay ( $5^{\text {th }}$ Period)
Richards (5th Period)

Richards (6th Period)

Cantwell ( $6^{\text {th }}$ Period)
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Problem 1 (35) $\qquad$
Problem 2 ( 35 ) $\qquad$
Problem 3 (30) $\qquad$

Total
(100) $\qquad$

## INSTRUCTIONS

- Closed book/notes exam. (Unit conversion page provided)
- Help sheet allowed. (8-1/2 $\times 11$ ' sheet of paper, one side)
- Laptops may be used; however, no pre-prepared worksheets or files may be used.

1) Show all work for complete credit.

- Start all problems at the ANALYSIS stage, but clearly label any information you use for your solution.
- Problems involving conservation or accounting principles MUST clearly identify the system and show a clear, logical progression from the basic principle(s).
- Don't expect us to read your mind as to how or why you did something in the solution. Clearly indicate how you arrived at your answer and how you used the given information in the process.
- Always crunch numbers last on an exam. The final numerical answer is worth the least amount of points. (Especially if all we would have to do is plug in the numbers into a well-documented solution.)

2) Useful Rule of Thumb (Heuristic): ( 100 point exam $) /(50 \mathrm{~min}) \approx 2$ point/minute. That means a 10 point problem is not worth more than 5 minutes of your time (at least the first time around).
3) Please remain seated until the end of class or everyone finishes. (Raise your hand and I'll pick up your exam if you have other work you need or want to do.)

| USEFUL INFORMATION | SI | USCS |  |
| :--- | :--- | :--- | :--- |
| Standard Acceleration of Gravity: | $g$ | $=9.810 \mathrm{~m} / \mathrm{s}^{2}$ | $=32.174 \mathrm{ft} / \mathrm{s}^{2}$ |
| Universal Ideal Gas Constant: | $R_{\mathrm{u}}$ | $=8.314 \mathrm{~kJ} /(\mathrm{kmol}-\mathrm{K})$ | $=1545(\mathrm{ft}-\mathrm{lbf}) /\left(\mathrm{lbmol}-{ }^{\circ} \mathrm{R}\right) \quad=1.986 \mathrm{Btu} /\left(\mathrm{lbmol}-{ }^{\circ} \mathrm{R}\right)$ |
|  |  |  |  |
| WATER (Liquid): | Density | $\rho$ | $=1000 \mathrm{~kg} / \mathrm{m}^{3}$ |
|  |  |  | $=62.4 \mathrm{lbm} / \mathrm{ft}^{3}=1.94 \mathrm{slug} / \mathrm{ft}^{3}$ |
| AIR: | Molecular weight | $M$ | $=28.97 \mathrm{~kg} / \mathrm{kmol}$ |
| AIR: | Specific gas constant | $R$ | $=0.287 \mathrm{~kJ} /(\mathrm{kg}-\mathrm{K})$ |

Problem 1 (40 points)
Nitrogen gas fills a piston-cylinder device as shown in the figure. The device contains 10 kilograms of nitrogen $\left(\mathrm{N}_{2}\right)$ gas initially at $P_{1}=120 \mathrm{kPa}$ and $T_{1}=300 \mathrm{~K}$.

During a constant-pressure expansion process, the gas volume doubles $\left(\forall_{2}=2 \forall_{1}\right)$.
Assume that nitrogen gas can be modeled as an ideal gas with constant, room-temperature specific heats:

$$
R=0.2968 \mathrm{~kJ} / / \mathrm{kg}-\mathrm{K} ; \quad c_{\mathrm{p}}=1.04 \mathrm{~kJ} / \mathrm{kg}-\mathrm{K} ; \quad c_{\mathrm{v}}=0.743 \mathrm{~kJ} / \mathrm{kg}-\mathrm{K}
$$

Determine the following:
(a) the work done by the gas on the piston during the expansion process, in kJ .
(b) the heat transfer of energy to the gas during this process, in kJ .


Problem 2 (35 points)
Two brine streams are mixed in a steady-state, adiabatic mixing chamber. Cold brine enters at Inlet 1 $\left(10^{\circ} \mathrm{C}\right.$ and 110 kPa$)$ and hot brine enters at Inlet $2\left(75^{\circ} \mathrm{C}\right.$ and 100 kPa$)$ with a mass flow rate of $10 \mathrm{~kg} / \mathrm{s}$. The product stream leaves at Outlet $3\left(20^{\circ} \mathrm{C}\right.$ and 100 kPa$)$.

A mechanical stirrer that rotates at 500 rpm enhances the steady mixing process. The shaft power input for the mechanical stirrer is 200 kW .

Experience shows that changes in kinetic and gravitational potential energy are negligible. You may also assume the brine, which is a liquid, can be modeled as an incompressible substance with constant, roomtemperature specific heats: $\rho=1150 \mathrm{~kg} / \mathrm{m}^{3}$ and $c=3.11 \mathrm{~kJ} / \mathrm{kg}-\mathrm{K}$.

Determine the following:
a) the mass flow rate of the cold brine stream, in $\mathrm{kg} / \mathrm{s}$.
b) the torque developed in the rotating shaft of the stirrer, in $\mathrm{kN}-\mathrm{m}$.

| 1 -- Cold brin | $\dot{W}_{\text {shaft }, \text { in }}=200 \mathrm{~kW} \quad L_{2 \ldots \text { Hot brine }}$ |
| :---: | :---: |
| $\dot{m}_{1}=$ ?? $\quad \dot{m}_{2}=10 \mathrm{~kg} / \mathrm{s}$ |  |
| $T_{1}=10^{\circ} \mathrm{C}$ |  |
| $P_{1}=110 \mathrm{kPa}$ | $\mathrm{P}_{2}=100 \mathrm{kPa}$ |
|  | 3-- Product |
|  | $\dot{m}_{3}=$ ? ${ }^{\text {a }}$ |
|  | $\downarrow \quad T_{3}=20^{\circ} \mathrm{C}$ |
|  | $P_{3}=100 \mathrm{kPa}$ |

Problem 3 (30 Points)
A block with mass $m$ is initially pushed against a spring compressing the spring length by $\delta$. When the block is released, the spring expands and the block slides up the inclined surface. (The block is not attached to the spring.)

The inclined surface has a coefficient of kinetic friction $\mu_{\mathrm{k}}$ and makes an angle $\theta$ with the horizontal as shown in the figure. The spring has a spring constant $k$.
Determine the speed $V$ of the block after it travels a distance $d$ up the inclined surface.
[SET UP the necessary equations but DO NOT SOLVE.]


## Length

$1 \mathrm{ft}=12 \mathrm{in}=0.3048 \mathrm{~m}=1 / 3 \mathrm{yd}$
$1 \mathrm{~m}=100 \mathrm{~cm}=1000 \mathrm{~mm}=39.37 \mathrm{in}=3.2808 \mathrm{ft}$
1 mile $=5280 \mathrm{ft}=1609.3 \mathrm{~m}$

## Mass

$1 \mathrm{~kg}=1000 \mathrm{~g}=2.2046 \mathrm{lbm}$
$1 \mathrm{lbm}=16 \mathrm{oz}=0.45359 \mathrm{~kg}$
1 slug $=32.174 \mathrm{lbm}$

## Temperature Values

$(\mathrm{T} / \mathrm{K})=\left(\mathrm{T} /{ }^{\circ} \mathrm{R}\right) / 1.8$
$(\mathrm{T} / \mathrm{K})=\left(\mathrm{T} /{ }^{\circ} \mathrm{C}\right)+273.15$
$\left(\mathrm{T} /{ }^{\circ} \mathrm{C}\right)=\left[\left(\mathrm{T} /{ }^{\circ} \mathrm{F}\right)-32\right] / 1.8$
$\left(\mathrm{T} /{ }^{\circ} \mathrm{R}\right)=1.8(\mathrm{~T} / \mathrm{K})$
$\left(\mathrm{T} /{ }^{\circ} \mathrm{R}\right)=\left(\mathrm{T} /{ }^{\circ} \mathrm{F}\right)+459.67$
$\left(\mathrm{T} /{ }^{\circ} \mathrm{F}\right)=1.8\left(\mathrm{~T} /{ }^{\circ} \mathrm{C}\right)+32$

## Temperature Differences

$\left(\Delta \mathrm{T} /{ }^{\circ} \mathrm{R}\right)=1.8(\Delta \mathrm{~T} / \mathrm{K})$
$\left(\Delta \mathrm{T} /{ }^{\circ} \mathrm{R}\right)=\left(\Delta \mathrm{T} /{ }^{\circ} \mathrm{F}\right)$
$(\Delta \mathrm{T} / \mathrm{K})=\left(\Delta \mathrm{T} /{ }^{\circ} \mathrm{C}\right)$

## Volume

$1 \mathrm{~m}^{3}=1000 \mathrm{~L}=10^{6} \mathrm{~cm}^{3}=10^{6} \mathrm{~mL}=35.315 \mathrm{ft}^{3}=264.17 \mathrm{gal}$
$1 \mathrm{ft}^{3}=1728 \mathrm{in}^{3}=7.4805 \mathrm{gal}=0.028317 \mathrm{~m}^{3}$
$1 \mathrm{gal}=0.13368 \mathrm{ft}^{3}=0.0037854 \mathrm{~m}^{3}$

## Volumetric Flow Rate

$1 \mathrm{~m}^{3} / \mathrm{s}=35.315 \mathrm{ft}^{3} / \mathrm{s}=264.17 \mathrm{gal} / \mathrm{s}$
$1 \mathrm{ft}^{3} / \mathrm{s}=1.6990 \mathrm{~m}^{3} / \mathrm{min}=7.4805 \mathrm{gal} / \mathrm{s}=448.83 \mathrm{gal} / \mathrm{min}$

## Force

$1 \mathrm{~N}=1 \mathrm{~kg} \cdot \mathrm{~m} / \mathrm{s}^{2}=0.22481 \mathrm{lbf}$
$1 \mathrm{lbf}=1 \mathrm{slug} \cdot \mathrm{ft} / \mathrm{s}^{2}=32.174 \mathrm{lbm} \cdot \mathrm{ft} / \mathrm{s}^{2}=4.4482 \mathrm{~N}$

## Pressure

$1 \mathrm{~atm}=101.325 \mathrm{kPa}=1.01325 \mathrm{bar}=14.696 \mathrm{lbf} / \mathrm{in}^{2}$
$1 \mathrm{bar}=100 \mathrm{kPa}=10^{5} \mathrm{~Pa}$
$1 \mathrm{~Pa}=1 \mathrm{~N} / \mathrm{m}^{2}=10^{-3} \mathrm{kPa}$
$1 \mathrm{lbf} / \mathrm{in}^{2}=6.8947 \mathrm{kPa}=6894.7 \mathrm{~N} / \mathrm{m}^{2}$ [lbf/in ${ }^{2}$ often abbreviated as "psi" ]

## Energy

$1 \mathrm{~J}=1 \mathrm{~N} \cdot \mathrm{~m}$
$1 \mathrm{~kJ}=1000 \mathrm{~J}=737.56 \mathrm{ft} \cdot \mathrm{lbf}=0.94782 \mathrm{Btu}$
$1 \mathrm{Btu}=1.0551 \mathrm{~kJ}=778.17 \mathrm{ft} \cdot \mathrm{lbf}$
$1 \mathrm{ft} \cdot \mathrm{lbf}=1.3558 \mathrm{~J}$

## Energy Transfer Rate

$1 \mathrm{~kW}=1 \mathrm{~kJ} / \mathrm{s}=737.56 \mathrm{ft} \cdot \mathrm{lbf} / \mathrm{s}=1.3410 \mathrm{hp}=0.94782 \mathrm{Btu} / \mathrm{s}$
$1 \mathrm{Btu} / \mathrm{s}=1.0551 \mathrm{~kW}=1.4149 \mathrm{hp}=778.17 \mathrm{ft} \cdot \mathrm{lbf} / \mathrm{s}$
$1 \mathrm{hp}=550 \mathrm{ft} \cdot \mathrm{lbf} / \mathrm{s}=0.74571 \mathrm{~kW}=0.70679 \mathrm{Btu} / \mathrm{s}$

## Specific Energy

$1 \mathrm{~kJ} / \mathrm{kg}=1000 \mathrm{~m}^{2} / \mathrm{s}^{2}$
$1 \mathrm{Btu} / \mathrm{lbm}=25037 \mathrm{ft}^{2} / \mathrm{s}^{2}$
$1 \mathrm{ft} \cdot \mathrm{lbf} / \mathrm{lbm}=32.174 \mathrm{ft}^{2} / \mathrm{s}^{2}$

