

"Problem 5.1 Limited Pressure Cycle.

This is a high compression diesel, so let's neglect residual mass"

$$f_{cv} = 0.5$$

$$f_{cp} = 1 - f_{cv}$$

"Engine Properties"

$$r_c = 15$$

"Fuel properties"

$$Q_{LHV} = 43000 \quad \text{"[kJ/lg]"}$$

$$FA = 0.045$$

$$AF = 1/FA$$

$$mfm = 1/(1+AF)$$

"Inlet Conditions - Point 1"

$$P_1 = 100$$

$$T_1 = 289$$

$$v_1 = \text{volume}(\text{Air}, T=T_1, P=P_1)$$

$$s_1 = \text{entropy}(\text{Air}, T=T_1, P=P_1)$$

$$u_1 = \text{intenergy}(\text{Air}, T=T_1)$$

$$\gamma_1 = CP(\text{Air}, T=T_1)/CV(\text{Air}, T=T_1)$$

"[kPa]"

"[K]"

"Point 2 Conditions"

$$s_2 = \text{entropy}(\text{Air}, T=T_2, P=P_2)$$

$$s_2 = s_1$$

$$v_2 = v_1/r_c$$

$$u_2 = \text{intenergy}(\text{Air}, T=T_2)$$

$$v_2 = \text{volume}(\text{Air}, T=T_2, P=P_2)$$

$$\gamma_2 = CP(\text{Air}, T=T_2)/CV(\text{Air}, T=T_2)$$

"Heat Added per Kg mixture - const vol - Point 3a Conditions"

$$q_{cv} = f_{cv} * mfm * Q_{LHV}$$

$$u_{3a} = \text{intenergy}(\text{Air}, T=T_{3a})$$

$$h_{3a} = \text{enthalpy}(\text{Air}, T=T_{3a})$$

$$q_{cv} = u_{3a} - u_2$$

$$P_{3a}/P_2 = T_{3a}/T_2$$

$$v_{3a} = v_2$$

$$\gamma_{3a} = CP(\text{Air}, T=T_{3a})/CV(\text{Air}, T=T_{3a})$$

"Heat Added per Kg mixture - constant press - Point 3b Conditions"

$$q_{cp} = f_{cp} * mfm * Q_{LHV}$$

$$h_{3b} = \text{enthalpy}(\text{Air}, T=T_{3b})$$

$$s_{3b} = \text{entropy}(\text{Air}, T=T_{3b}, P=P_{3b})$$

$$u_{3b} = \text{intenergy}(\text{Air}, T=T_{3b})$$

$$q_{cp} = h_{3b} - h_{3a}$$

$$P_{3b} = P_{3a}$$

$$P_{3b} * v_{3b} = R * T_{3b}$$

$$v_{3b}/v_{3a} = T_{3b}/T_{3a}$$

$$\gamma_{3b} = CP(\text{Air}, T=T_{3b})/CV(\text{Air}, T=T_{3b})$$

"Point 4 Conditions"

$$v_4 = v_2 * r_c$$

$$v_4 = \text{volume}(\text{Air}, T=T_4, P=P_4)$$

$$s_4 = \text{entropy}(\text{Air}, T=T_4, P=P_4)$$

$$s_{3b} = s_4$$

$$u_4 = \text{intenergy}(\text{Air}, T=T_4)$$

$$\gamma_4 = \text{CP}(\text{Air}, T=T_4) / \text{CV}(\text{Air}, T=T_4)$$

"Totals of Heat Added and work done"

$$q_{\text{add}} = q_{\text{cv}} + q_{\text{cp}}$$

$$w_{\text{comp}} = u_2 - u_1$$

$$w_{\text{exp}} = p_{3b} * (v_{3b} - v_{3a}) + u_{3b} - u_4$$

$$w_{\text{net}} = w_{\text{exp}} - w_{\text{comp}}$$

"Fuel Conversion Efficiency"

$$\eta_f = w_{\text{net}} / q_{\text{add}}$$

$$\gamma = (\gamma_1 + \gamma_2 + \gamma_{3a} + \gamma_{3b} + \gamma_4) / 5$$

$$\eta_{f1} = 1 - (T_4 - T_1) / ((T_{3a} - T_2) + \gamma * (T_{3b} - T_{3a}))$$

$$\beta = v_{3b} / v_{3a}$$

$$\alpha = P_{3a} / P_2$$

$$\eta_{f2} = 1 - 1 / r_c^{(\gamma - 1)} * ((\alpha * \beta^\gamma - 1) / (\alpha * \gamma * (\beta - 1) + \alpha - 1))$$

$$pr = P_{3a} / P_1$$

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Engine Properties

$$r_c = 15$$

Fuel properties

$$Q_{\text{LHV}} = 43000 \text{ [kJ/kg]}$$

$$FA = 0.045$$

$$AF = \frac{1}{FA}$$

$$m_{\text{fm}} = \frac{1}{1 + AF}$$

Inlet Conditions - Point 1

$$P_1 = 100 \text{ [kPa]}$$

$$T_1 = 289 \text{ [K]}$$

$$v_1 = v[\text{'Air'}, T=T_1, P=P_1]$$

$$s_1 = s[\text{'Air'}, T=T_1, P=P_1]$$

$$u_1 = u[\text{'Air'}, T=T_1]$$

$$\gamma_1 = \frac{Cp[\text{'Air'}, T=T_1]}{Cv[\text{'Air'}, T=T_1]}$$

Point 2 Conditions

$$s_2 = s[\text{'Air'}, T=T_2, P=P_2]$$

$$s_2 = s_1$$

$$v_2 = \frac{v_1}{r_c}$$

$$u_2 = u[\text{'Air'}, T=T_2]$$

$$v_2 = v[\text{'Air'}, T=T_2, P=P_2]$$

$$\gamma_2 = \frac{Cp[\text{'Air'}, T=T_2]}{Cv[\text{'Air'}, T=T_2]}$$

Heat Added per Kg mixture - const vol - Point 3a Conditions

$$q_{cv} = f_{cv} \cdot m_{fm} \cdot Q_{LHV}$$

$$u_{3a} = u[\text{'Air'}, T=T_{3a}]$$

$$h_{3a} = h[\text{'Air'}, T=T_{3a}]$$

$$q_{cv} = u_{3a} - u_2$$

$$\frac{P_{3a}}{P_2} = \frac{T_{3a}}{T_2}$$

$$v_{3a} = v_2$$

$$\gamma_{3a} = \frac{Cp[\text{'Air'}, T=T_{3a}]}{Cv[\text{'Air'}, T=T_{3a}]}$$

Heat Added per Kg mixture - constant press - Point 3b Conditions

$$q_{cp} = f_{cp} \cdot m_{fm} \cdot Q_{LHV}$$

$$h_{3b} = h[\text{'Air'}, T=T_{3b}]$$

$$s_{3b} = s[\text{'Air'}, T=T_{3b}, P=P_{3b}]$$

$$u_{3b} = u[\text{'Air'}, T=T_{3b}]$$

$$q_{cp} = h_{3b} - h_{3a}$$

$$P_{3b} = P_{3a}$$

$$P_{3b} \cdot v_{3b} = R \cdot T_{3b}$$

$$\frac{v_{3b}}{v_{3a}} = \frac{T_{3b}}{T_{3a}}$$

$$\gamma_{3b} = \frac{Cp[\text{'Air'}, T=T_{3b}]}{Cv[\text{'Air'}, T=T_{3b}]}$$

Point 4 Conditions

$$v_4 = v_2 \cdot r_c$$

$$v_4 = v[\text{'Air'}, T=T_4, P=P_4]$$

$$s_4 = s[\text{'Air'}, T=T_4, P=P_4]$$

$$s_{3b} = s_4$$

$$u_4 = u[\text{'Air'}, T=T_4]$$

$$\gamma_4 = \frac{Cp[\text{'Air'}, T=T_4]}{Cv[\text{'Air'}, T=T_4]}$$

Totals of Heat Added and work done

$$q_{add} = q_{cv} + q_{cp}$$

$$w_{comp} = u_2 - u_1$$

$$w_{exp} = P_{3b} \cdot [v_{3b} - v_{3a}] + u_{3b} - u_4$$

$$w_{net} = w_{exp} - w_{comp}$$

Fuel Conversion Efficiency

$$\eta_f = \frac{w_{net}}{q_{add}}$$

$$\gamma = \frac{\gamma_1 + \gamma_2 + \gamma_{3a} + \gamma_{3b} + \gamma_4}{5}$$

$$\eta_{f1} = 1 - \left[\frac{T_4 - T_1}{T_{3a} - T_2 + \gamma \cdot (T_{3b} - T_{3a})} \right]$$

$$\beta = \frac{v_{3b}}{v_{3a}}$$

$$\alpha = \frac{P_{3a}}{P_2}$$

$$\eta_{f2} = 1 - \left[\frac{1}{r_c^{(\gamma - 1)}} \cdot \left(\frac{\alpha \cdot \beta^\gamma - 1}{\alpha \cdot \gamma \cdot [\beta - 1] + \alpha - 1} \right) \right]$$

$$pr = \frac{P_{3a}}{P_1}$$

Unit Settings: [kJ]/[K]/[kPa]/[kg]/[radians]

| | | | |
|-------------------------------------|----------------------|-------------------------|---------------------------|
| AF = 22.22 | $\alpha = 2.264$ | $\beta = 1.398$ | $\eta_f = 0.5798$ |
| $\eta_{f1} = 0.5183$ | $\eta_{f2} = 0.5817$ | FA = 0.045 | $f_{cp} = 0.5$ |
| $f_{cv} = 0.5$ | $\gamma = 1.333$ | $\gamma_1 = 1.399$ | $\gamma_2 = 1.352$ |
| $\gamma_{3a} = 1.301$ | $\gamma_{3b} = 1.29$ | $\gamma_4 = 1.321$ | $h_{3a} = 2062$ |
| $h_{3b} = 2988$ | mfm = 0.04306 | pr = 95.91 | $P_1 = 100$ [kPa] |
| $P_2 = 4236$ | $P_{3a} = 9591$ | $P_{3b} = 9591$ | $P_4 = 435.2$ |
| $q_{add} = 1852$ | $q_{cp} = 925.8$ | $q_{cv} = 925.8$ | $Q_{LHV} = 43000$ [kJ/kg] |
| $R = 0.287$ [kJ/(kg-K)] | $r_c = 15$ | $s_1 = 5.664$ [kJ/kg-K] | $s_2 = 5.664$ [kJ/kg-K] |
| $s_{3b} = 6.811$ | $s_4 = 6.811$ | $T_1 = 289$ [K] | $T_2 = 816.2$ |
| $T_{3a} = 1848$ | $T_{3b} = 2583$ | $T_4 = 1258$ | $u_1 = 206.4$ [kJ/kg] |
| $u_2 = 605.6$ | $u_{3a} = 1531$ | $u_{3b} = 2246$ | $u_4 = 984.5$ |
| $v_1 = 0.8295$ [m ³ /kg] | $v_2 = 0.0553$ | $v_{3a} = 0.0553$ | $v_{3b} = 0.07729$ |
| $v_4 = 0.8295$ | $w_{comp} = 399.2$ | $w_{exp} = 1473$ | $w_{net} = 1074$ |

Parametric Table: Table 2

| | η_f | f_{cv} |
|--------|----------|----------|
| Run 1 | 0.4969 | 0 |
| Run 2 | 0.5286 | 0.1 |
| Run 3 | 0.549 | 0.2 |
| Run 4 | 0.563 | 0.3 |
| Run 5 | 0.5728 | 0.4 |
| Run 6 | 0.5798 | 0.5 |
| Run 7 | 0.5847 | 0.6 |
| Run 8 | 0.588 | 0.7 |
| Run 9 | 0.5901 | 0.8 |
| Run 10 | 0.5913 | 0.9 |
| Run 11 | 0.5916 | 1 |

